

Setting the Standard for Automation™



ISA Symposium

Alarm Management & High Performance HMI

Hector R. Perez

Standards
Certification
Education & Training
Publishing
Conferences & Exhibits

April 14th, 2011
League City

Agenda



- About the presenter and PAS
- Human Reliability
- Alarm Management
- High Performance HMI
- Questions

- Human Machine Interface experience
- Alarm Management experience
- HMI Product Management
 - Software inception and development
 - Intellectual property
 - Path finding
 - Product integration



About PAS



- Founded in 1993
 - Operations Effectiveness
 - Alarm Management
 - High-Performance HMI
 - Control Loop Performance
 - Automation Effectiveness
 - Automation Systems Integrity
 - Disaster Recovery
 - Knowledge Retention/Collaboration
- Industry Organizations & Strategic Partners
 - Voting Member of the ISA18 committee
 - EPRI, ISA, API, AICHE, NPRA, EEMUA



Why Alarm Management & HP HMI?



To improve *human reliability* and enable *safe production*!

What is *human reliability*?

- Human reliability is related to human factors that help minimize human error and lead to optimum human performance.

How do we do it?

- We achieve this by aggregating, contextualizing and simplifying essential information and making it universally accessible and useful.

What is the benefit?

- Improved safety, reliability, productivity and knowledge retention.

Manufacturing Value



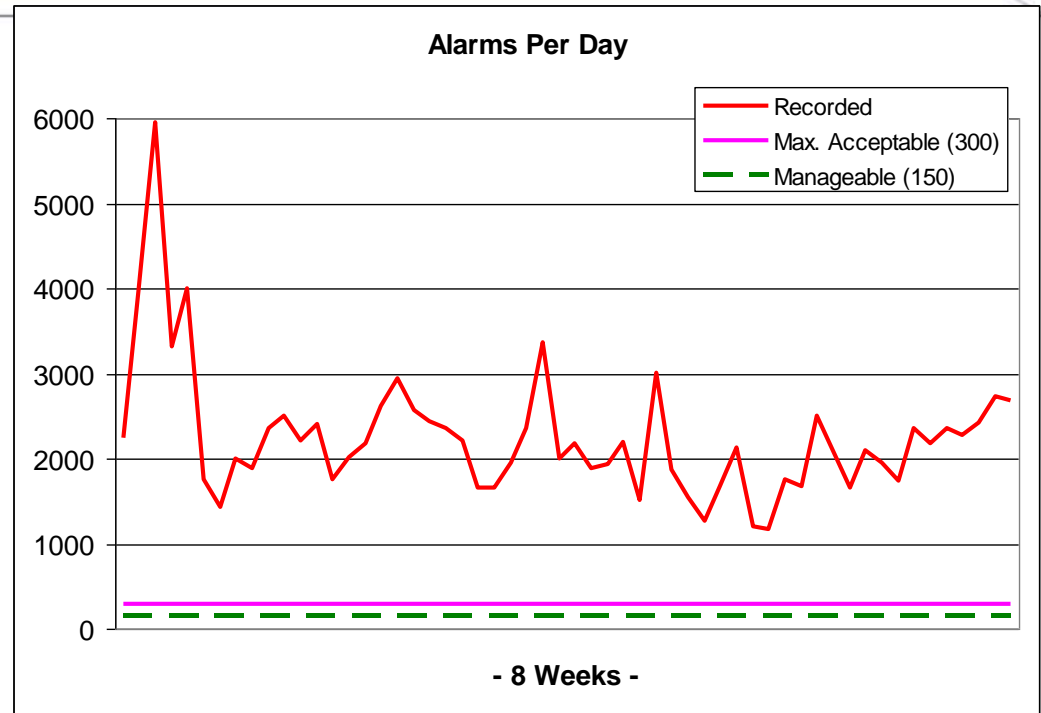
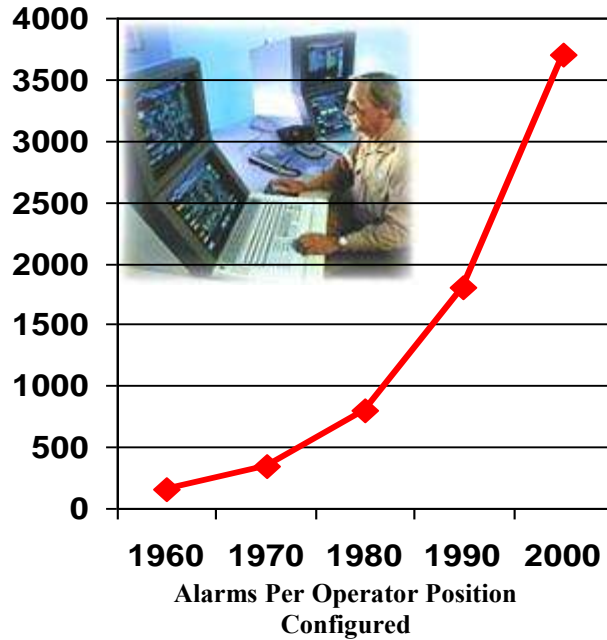
- **Alarms**
- **HMI**
- **Control Loop**



Outside of R&D, manufacturing is the only segment of a company's supply chain where value is added.

Manufacturing is the largest financial lever under a company's control.

Alarm Management



Thousands of Alarm Events Presented to the Operator!

Human Reliability: Do NOT miss the important alarm

Alarm Management – 7 steps



Step 1: Develop, Adopt and Maintain an Alarm Philosophy

Step 2: Collect Data And Benchmark Your Systems

Step 3: Perform “Bad Actor” Alarm Resolution

Step 4: Perform Alarm Documentation and Rationalization

Step 5: Implement Alarm Audit and Enforcement Technology

Step 6: Implement Real Time Alarm Management

Step 7: Control and Maintain Your Improved System

Step 1 – Alarm Philosophy



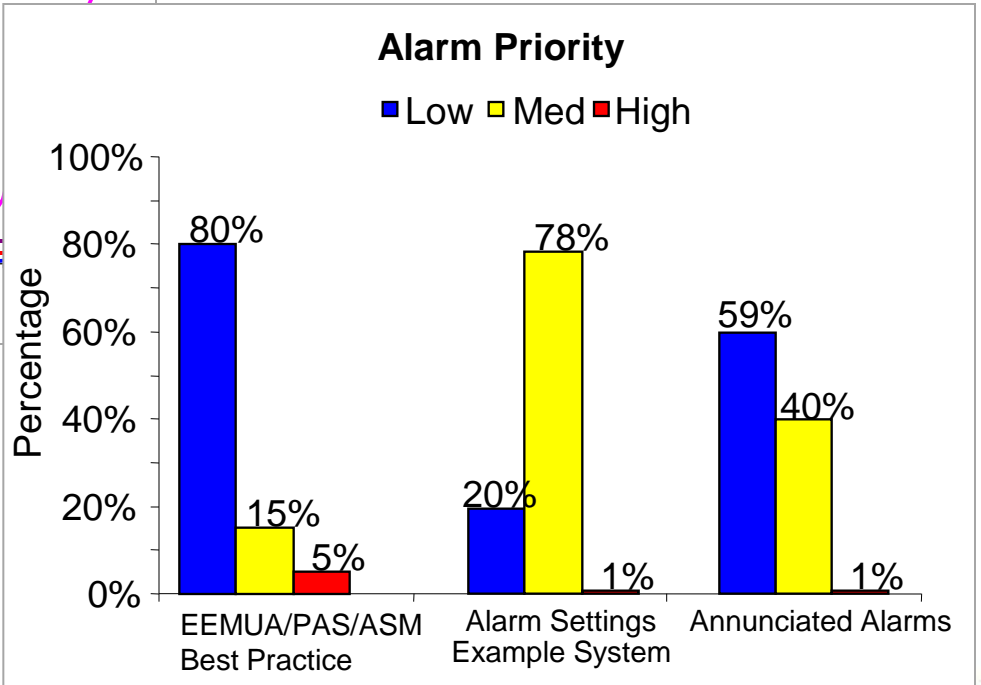
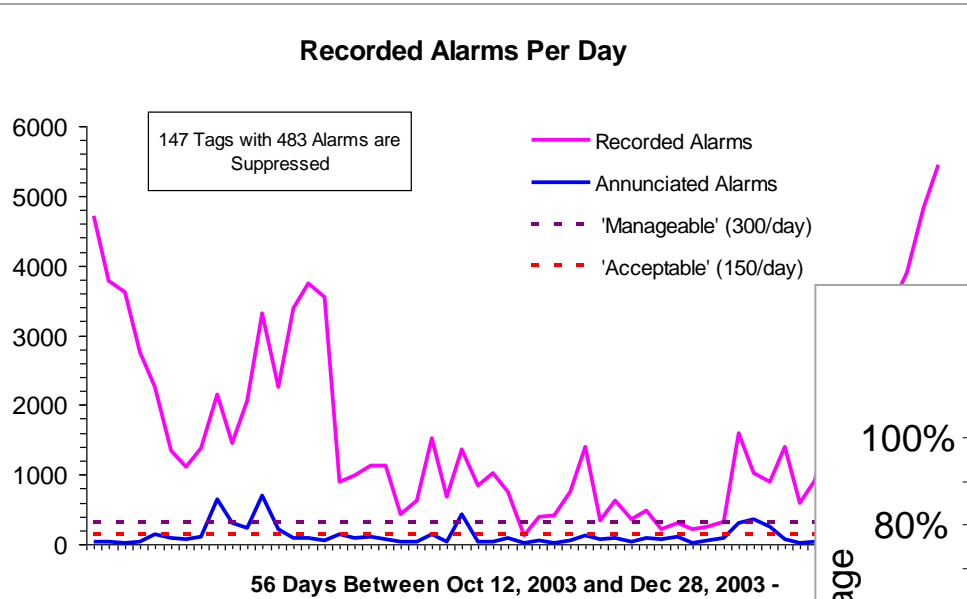
- Alarm Design Guideline Based on Best Practices
 - Alarm Selection – What is an alarm?
 - Priority determination & Distribution - Methodology
 - Configuration
 - KPIs
 - Nuisance Alarm Resolution
 - State Based Alarming
 - Alarm Shelving

Simplify access to accepted best practices

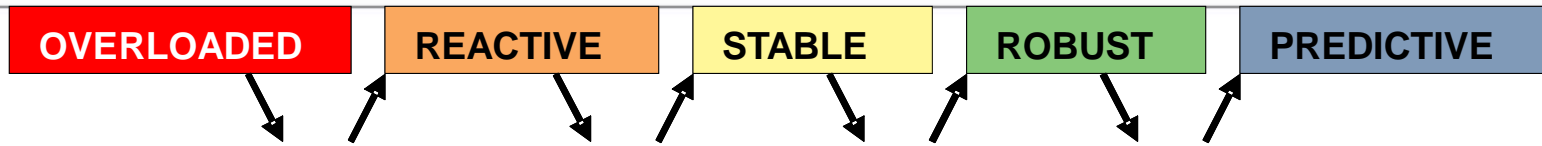
Step 2 - Benchmarking



- Is my Alarm system performing as per accepted best practices?



Benchmarking - Robust



Improvement Plans : Specific Steps to move from each classification to the next.

- **ROBUST**: Average and the peak alarm rates are under control for foreseeable plant operating scenarios
 - Dynamic and state-based techniques used to improve the real time performance
 - Alarm system is reliable during all plant modes, including normal operation and plant upsets
 - Alarm system configuration is not subject to inadvertent change

Operators have a high degree of confidence in the alarm system, and have time to detect and understand all alarms.

Step 3 – Bad Actor Resolution

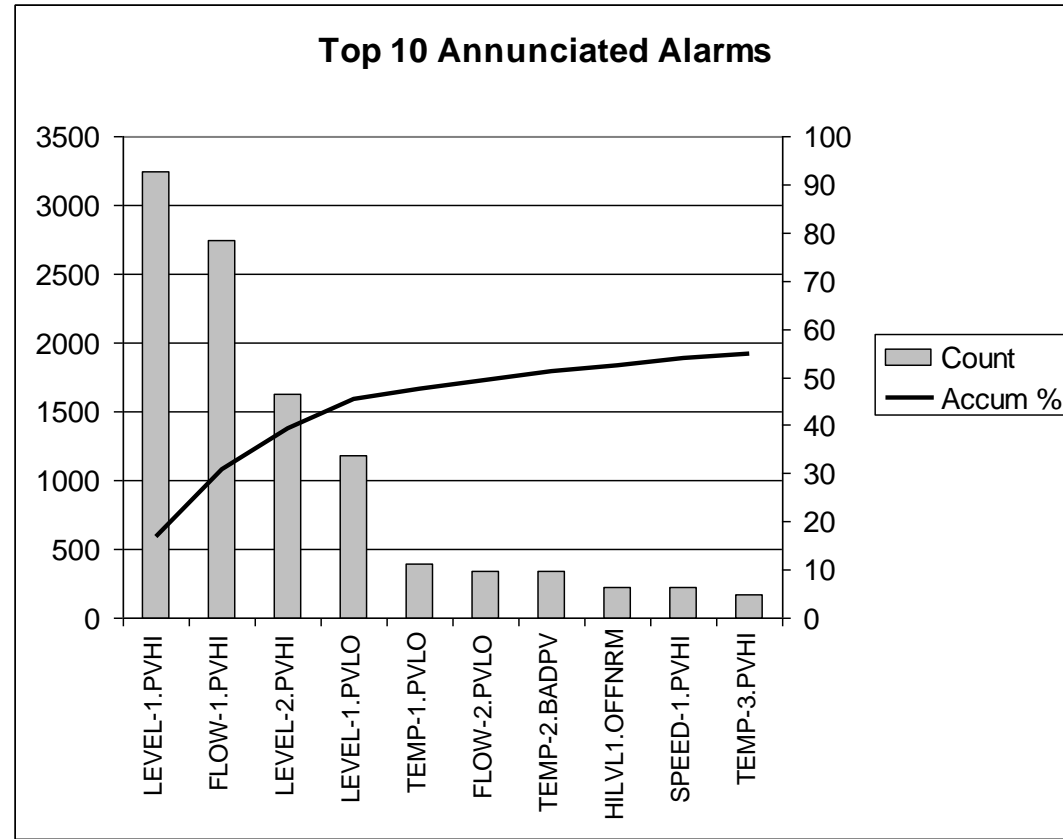


- Bad Actor = Nuisance or meaningless alarms

- Chattering alarms
- Fleeting alarms
- Stale alarms
- Duplicate alarms
- No Action alarms

- Correction Methods:

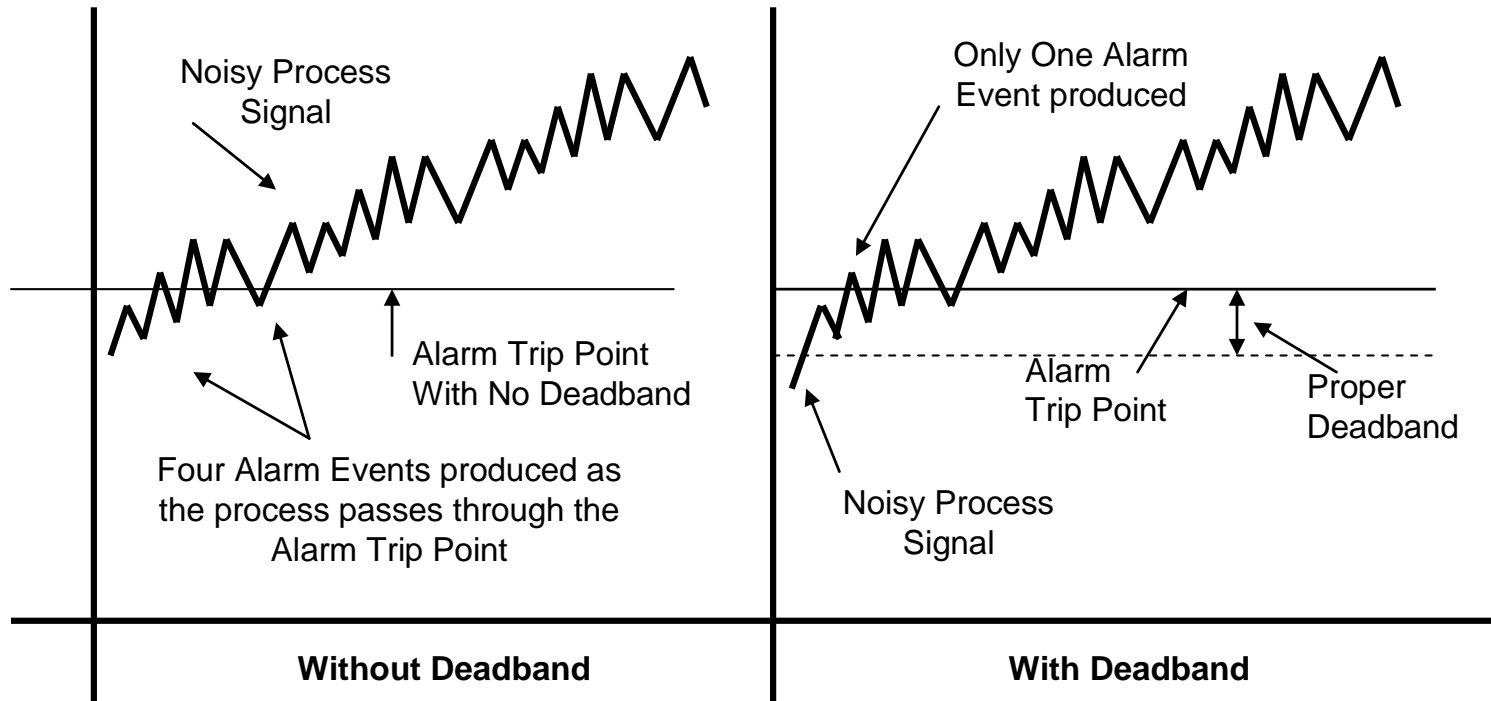
- Dead Band
- Time-Delay
- PV Filtering
- Alarm Shelving



Deadband and Alarms



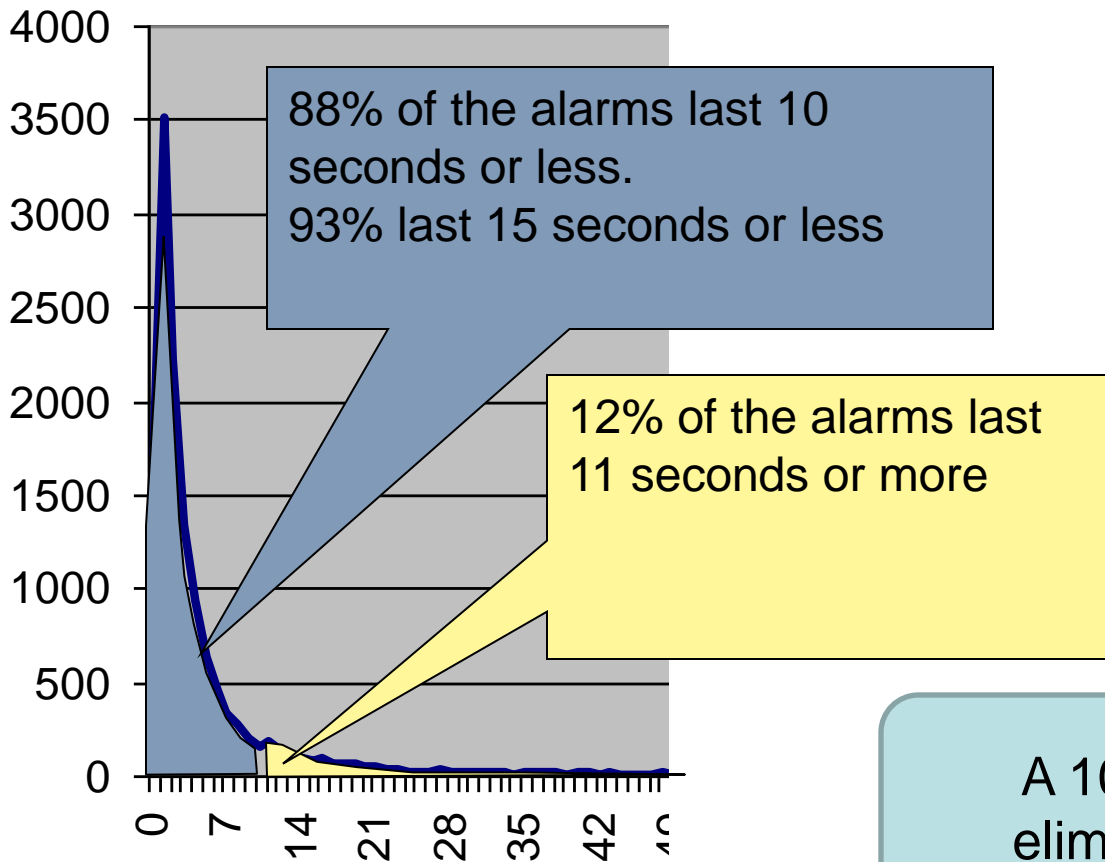
- EVERY analog alarm needs a deadband or it will chatter. All process signals have noise.



Alarm Reduction- ON-Delay



- The AREA UNDER THE CURVE totals 100% of the alarms:



A 10 second ON-Delay would eliminate 88% of these alarms

Step 4 – Alarm Documentation & Rationalization



- Evaluate Every Possible Alarm To Ensure Compliance with the Alarm Philosophy:
 - All Alarms Require Operator Action
 - Alarms are based on the best indicator of the root cause of an abnormal situation (and not duplicated)
 - All Alarms must be produced upon abnormal situations only, not from normal situations
 - Alarm Settings (not just trip points) are properly designed
 - Alarm Priorities are based on a sound and consistent methodology
 - Eliminate combination alarms



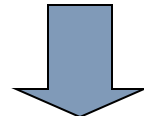
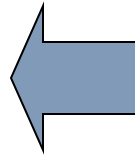
Priority Determination



Typical Grid-Based Priority Determination:

Impact Category	NONE	MINOR	MAJOR	SEVERE
Personnel	No injury or health effect	Alarms where operator action is the primary method by which harm to a person is avoided shall be configured at the highest DCS priority		
Public or Environment	No effect	Minimal exposure. No impact. Does not cross fence line. Contained release. Little, if any, clean up. Source eliminated. Negligible financial consequences.	Exposed to hazards that may cause injury. Hospitalizations and medical first aid possible. Damage Claims. Contamination causes some non-permanent damage.	Uncontained release of hazardous materials with major environmental impact and 3 rd party impact. Exposed to life-threatening hazard. Disruption of basic services. Impact involving the community. Catastrophic property damage. Extensive cleanup measures and financial consequences.
Costs or Value of Production Loss	No loss	Event costing <\$10,000, notification only at Department Head level	Event costing \$10,000 - \$100,000, notification at Site Manager level	Event costing >\$100,000, notification above Site Manager level

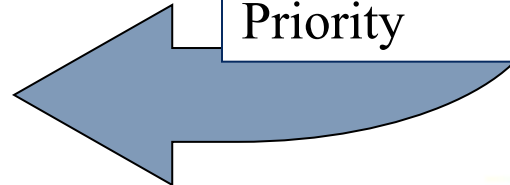
Severity of Consequence, Plus:



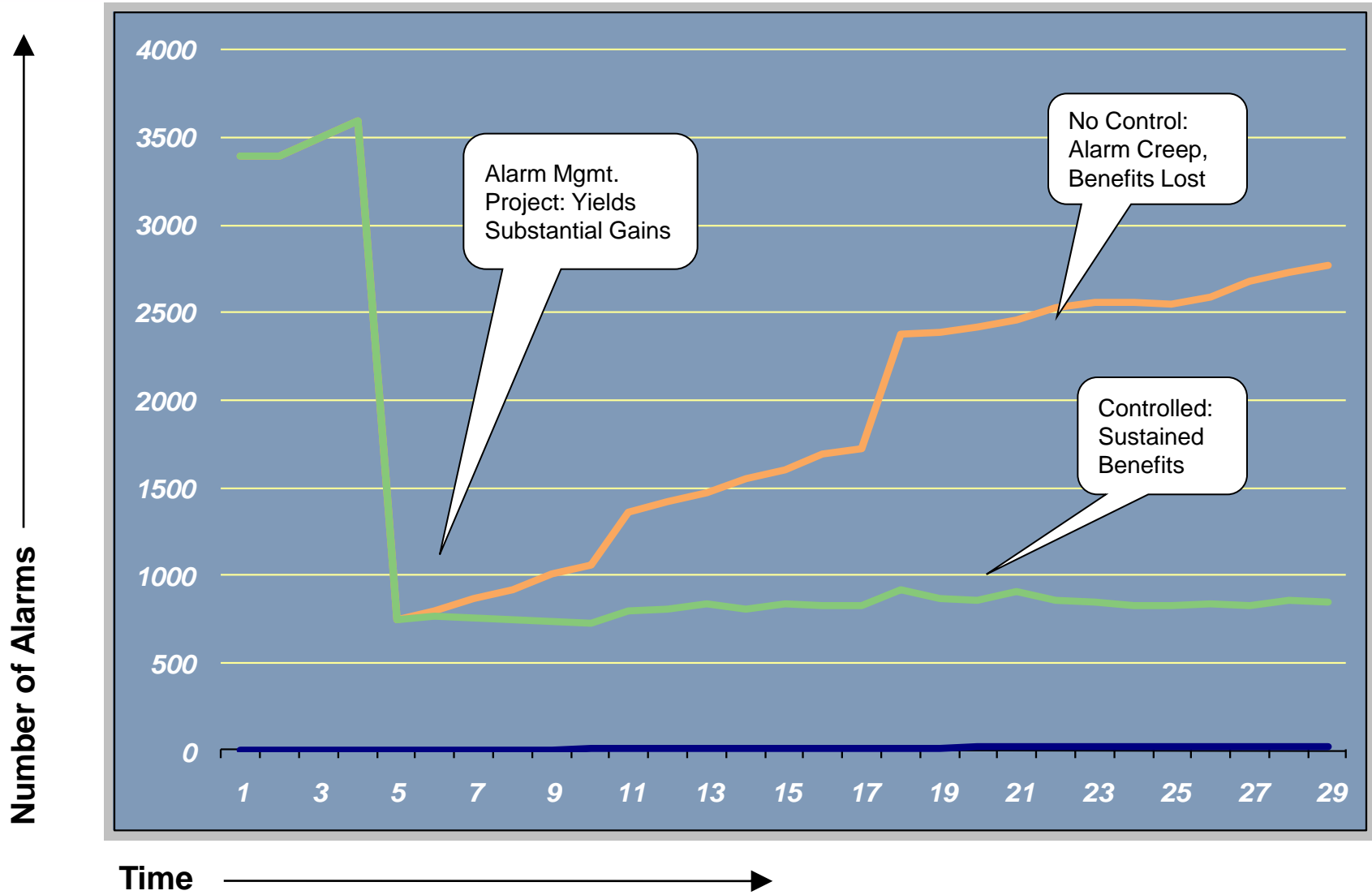
Time Available to Respond
> 30 Minutes
10 - 30 Minutes
3 - 10 Minutes
<3 Minutes

Alarm Priority Determination				
Time Available	Severity of Consequences			
	None	Minor	Major	Severe
>30 Min	No Alarm	Re-engineer the Alarm for Urgency		
10-30 Min	No Alarm	LOW	LOW	MED
3-10 Min	No Alarm	LOW	MED	MED
<3 Min	No Alarm	MED	HIGH	HIGH

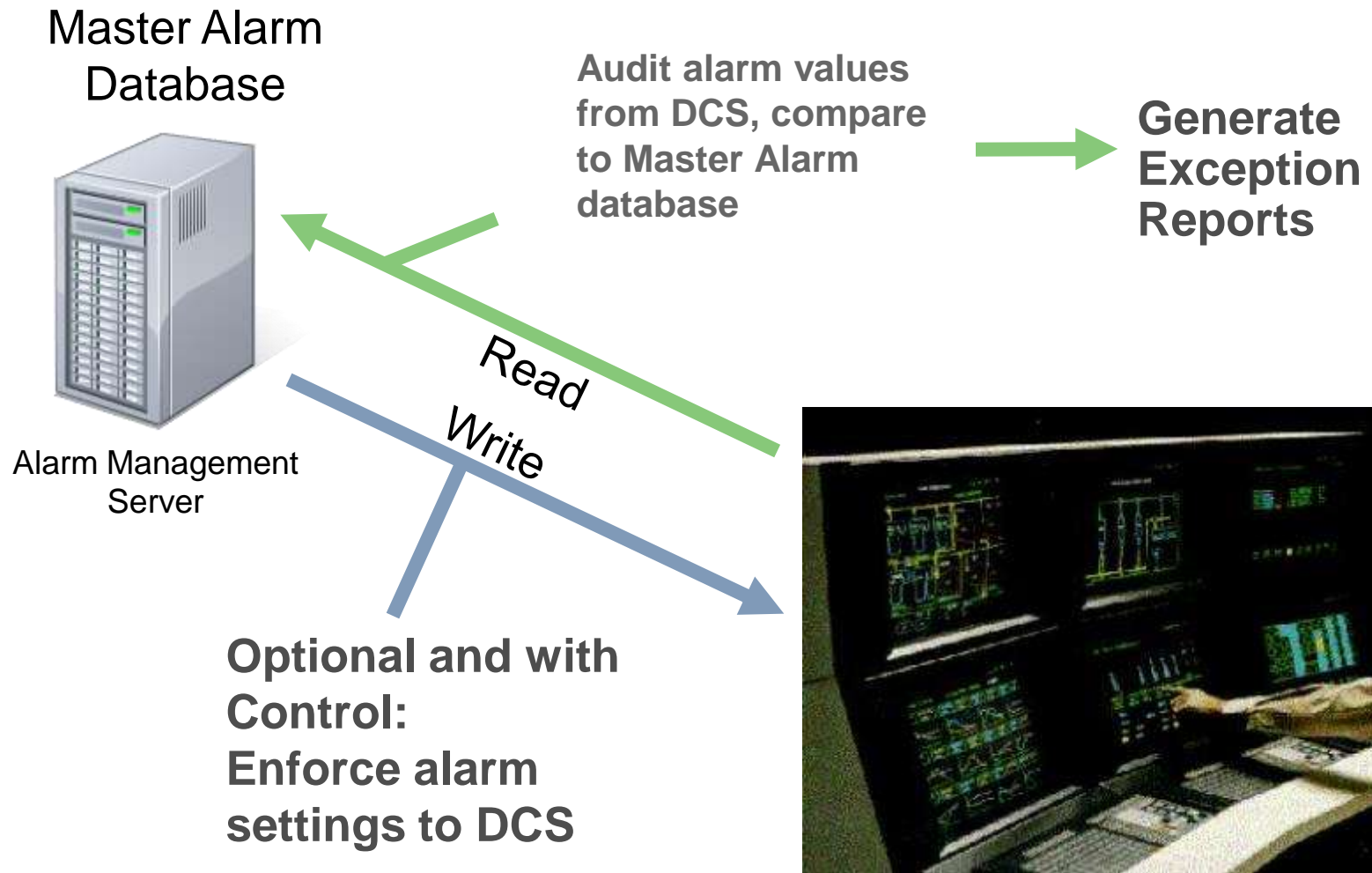
Determines Alarm Priority



Step 5 – Audit and Enforce



Alarm Audit and Enforce



Review and approve changes

Step 6 – Real-Time Alarm Management

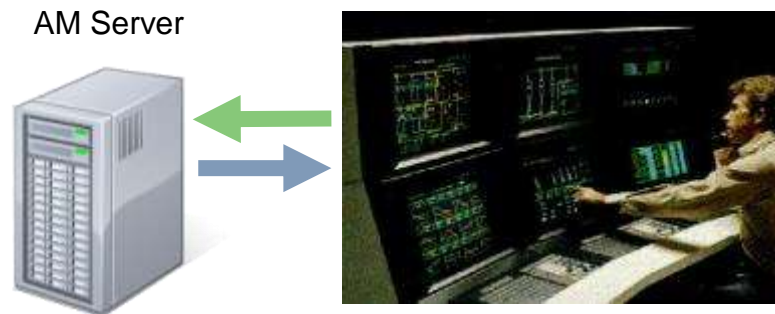
If your process:

- Makes Multiple Products or Grades
- Uses Multiple Differing Feedstocks
- Has Parallel Operating Trains
- Has Different Modes of Operation
- Runs at Different Rates

Then:

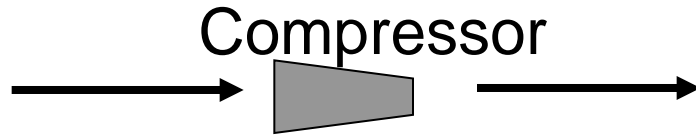
- Don't have only ONE set of unchanging, compromise alarms settings for your alarms.

State-based alarming technology, lets you have multiple alarm settings that are optimum and correct for all your operating conditions.



It is NOT OK to ignore an alarm

Alarm Flood Suppression – Shutdown State



States:
RUNNING (default)
and
SHUTDOWN

When the State is **SHUTDOWN**, suppress the following alarms:

- Low Flow*
- Low Discharge Pressure*
- High Suction Pressure*
- Low Oil Pressure*
- Low Amps*
- Low Speed*
- Several BAD VALUE alarms*

...and so forth – the ***expected diagnostics*** plus closely related, **expected** process alarms.

Post-Shutdown, the **important** alarms are from the remainder of the process as it adjusts to the loss of the compressor

Step 7 – Control and Maintain Your System



- The following types of changes to alarms must be controlled:
 - Changes in alarm priority
 - Changes in alarm trip point
 - Creation of new alarms
 - Deletion of existing alarms
 - Change of alarm type
 - Change of alarm description or text message
 - Temporary suppression of alarms (an approved Shelving methodology must be used)
 - Point execution status (turning a sensor “on” or “off”)
 - Changes in alarm presentation on graphics
 - Additions of, modifications to, or updates to alarm handling capabilities such as Alarm Shelving systems or State-Based Alarming configuration
- The following changes should be controlled as well
 - Controller tuning parameters
 - Point ranges
 - Modification of logic points, interlocks, embedded programs, DCS operating system software, and similar functions

Your Alarms are Now Under Control



Date/Time	Source	Type	Source Page	Source	Priority	Description	PV	Alarm	Lead	Value	From	To
10/04/05 14:41:45	Alarm	CONTROL	TR	ALDR001	HIGH	MAX TEMP	24.0000	PV ALARM	HIGH	21.0000		
10/04/05 14:44:44	Alarm	CONTROL	TR	ALDR001	HIGH	MAX TEMP	24.0000	PV ALARM	DOWN	22.0000		
10/04/05 14:44:38	Alarm	CONTROL	TR	ALDR001	ALDR001	MAX TEMP	24.0000	PV ALARM	HIGH	RETURN		
10/04/05 17:00:33	SiteA	ALARM	CONTROL	R1T0TOP	ALDR001	TOP TEMPERATURE	64.0000	PV ALARM	HIGH	22.0000		
10/04/05 14:59:38	Alarm	CONTROL	TR	ALDR001	ALDR001	MAX TEMP	22.0000	PV ALARM	HIGH	22.0000		
10/04/05 14:59:03	Alarm	CONTROL	TR	CONSOLE	CONSOLE	SANDBATH 2 MET SP	480.2718	PV ALARM	HIGH	100.0000		
10/04/05 14:58:49	Alarm	CONTROL	TR	CONSOLE	CONSOLE	SANDBATH 2 MET SP	50.2000	PV ALARM	HIGH	RETURN		
10/04/05 14:35:48	SiteA	ALARM	CONTROL	R1COOLSV	ALDR001	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		
10/04/05 14:35:34	SiteA	ALARM	CONTROL	R1COOLSV	ALDR001	R1 COOLANT BUX VALVE	CL0001	DIGALARM	STATE	RETURN		
10/04/05 14:34:24	SiteA	ALARM	CONTROL	R1COOLSV	ALDR001	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		
10/04/05 14:34:25	SiteA	ALARM	CONTROL	R1COOLSV	ALDR001	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	RETURN		
10/04/05 14:50:25	SiteA	ALARM	CONTROL	SLPWSGHT	ALDR001	SLOP TANK WEIGHT	5549.942	PV ALARM	HIGH	6000.000		
10/04/05 14:50:20	SiteA	ALARM	CONTROL	SLPWSGHT	ALDR001	SLOP TANK WEIGHT	4630.028	PV ALARM	HIGH	RETURN		
10/04/05 14:36:18	Alarm	CONTROL	TR	ALDR001	ALDR001	MAX TEMP	22.0000	PV ALARM	HIGH	RETURN		
10/04/05 14:35:48	Alarm	CONTROL	TR	ALDR001	ALDR001	MAX TEMP	22.0000	PV ALARM	DOWN	RETURN		
10/04/05 14:35:28	Alarm	CONTROL	TR	ALDR001	ALDR001	MAX TEMP	22.0000	PV ALARM	DOWN	60.0000		
10/04/05 14:34:44	Alarm	CONTROL	TR	ALDR001	ALDR001	MAX TEMP	22.0000	PV ALARM	HIGH	15.0000		
10/04/05 14:31:23	Alarm	CONTROL	TR	ALDR001	ALDR001	MAX TEMP	24.0000	PV ALARM	HIGH	RETURN		
10/04/05 14:31:08	Alarm	CONTROL	TR	ALDR001	ALDR001	MAX TEMP	22.0000	PV ALARM	HIGH	25.0000		
10/04/05 14:30:57	SiteA	ALARM	CONTROL	R2TEMPHH	ALDR001	R 2 TEMP HEAT REQ.	141.1301	PV ALARM	HIGH	125.0000		
10/04/05 14:25:18	SiteA	ALARM	CONTROL	R1T0TOP	ALDR001	TOP TEMPERATURE 107 7994	RET.	PV ALARM	HIGH			
10/04/05 14:22:07	SiteA	ALARM	CONTROL	R1T0TOP	ALDR001	TOP TEMPERATURE	200.7576	PV ALARM	HIGH	200.0000		
10/04/05 14:17:17	SiteA	ALARM	CONTROL	R1T0TOP	ALDR001	TOP TEMPERATURE 84 0000B	RET.	PV ALARM	HIGH			
10/04/05 14:16:18	SiteA	ALARM	CONTROL	R1COOLSV	ALDR001	R1 COOLANT BUX VALVE	CLOSEC	DIGALARM	STATE	OPEN		
10/04/05 14:09:27	SiteA	ALARM	CONTROL	R1T0TOP	ALDR001	TOP TEMPERATURE	94.0000	PV ALARM	HIGH	31.0000		
10/04/05 14:07:48	SiteA	ALARM	CONTROL	R1COOLSV	ALDR001	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		

7 Steps of Alarm Management

- Alarm system is reliable during all plant modes
- Operators have a high degree of confidence in the alarm system, and have time to detect all alarms
- Alarm system configuration is not subject to inadvertent change

Date/Time	Source	Type	Source Page	Source	Priority	Description	PV	Alarm	Lead	Value	From	To
10/04/05 14:41:45	Alarm	CONTROL	TR	ALDR001	HIGH	MAX TEMP	24.0000	PV ALARM	HIGH	21.0000		

Your Alarms are Now Under Control



Date/Time	Source	Type	Source Pgm	Source	Priority	Description	PV	Alarm	Lead	Value	From	To
10/04/05 14:41:45	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	24.0000	PV ALARM	HIGH	21.0000		
10/04/05 14:44:44	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	24.0000	PV ALARM	CRIT	22.0000		
10/04/05 14:44:38	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	24.0000	PV ALARM	HIGH	RETURN		
10/04/05 17:00:33	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE	64.0000	PV ALARM	HIGH	22.0000		
10/04/05 14:59:38	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	22.0000		
10/04/05 14:59:01	Alarm01	ALARM	CONTROL	TRN	CONTROL	SANDBATH 2 HD SP	480.2718	PV ALARM	HIGH	100.0000		
10/04/05 14:58:49	Alarm01	ALARM	CONTROL	TRN	CONTROL	SANDBATH 2 HD SP	50.2000	PV ALARM	HIGH	RETURN		
10/04/05 14:35:48	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		
10/04/05 14:35:34	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	CLD001	DIGALARM	STATE	RETURN		
10/04/05 14:34:24	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		
10/04/05 14:34:25	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	RETURN		
10/04/05 15:00:25	Stella	ALARM	CONTROL	SLPWSHT	ALARM01	SLOP TANK WEIGHT	5545.952	PV ALARM	HIGH	6000.000		
10/04/05 15:00:23	Stella	ALARM	CONTROL	SLPWSHT	ALARM01	SLOP TANK WEIGHT	4630.028	PV ALARM	HIGH	RETURN		
10/04/05 15:36:18	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	RETURN		
10/04/05 15:35:48	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	LOW	RETURN		
10/04/05 15:35:28	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	98.0000		
10/04/05 15:34:44	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	15.0000		
10/04/05 15:31:23	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	34.0000	PV ALARM	HIGH	RETURN		
10/04/05 15:20:58	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	25.0000		
10/04/05 14:30:57	Stella	ALARM	CONTROL	R2TEMP.HD	ALARM01	R 2 TEMP HEAT REQ.	141.1301	PV ALARM	HIGH	125.0000		
10/04/05 14:25:18	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE 107 T994	RET.	PV ALARM	HIGH			
10/04/05 14:22:07	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE	200.7578	PV ALARM	HIGH	200.0000		
10/04/05 14:17:17	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE 8400038	RET	PV ALARM	HIGH			
10/04/05 14:16:18	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE CLOSED		DIGALARM	STATE			
10/04/05 14:09:27	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE	94.0000	PV ALARM	HIGH	31.0000		
10/04/05 14:07:48	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		

Date/Time	Source	Type	Source Pgm	Source	Priority	Description	PV	Alarm	Lead	Value	From	To
10/04/05 14:41:45	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	24.0000	PV ALARM	HIGH	21.0000		
10/04/05 14:44:44	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	24.0000	PV ALARM	CRIT	22.0000		
10/04/05 14:44:38	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	24.0000	PV ALARM	HIGH	RETURN		
10/04/05 17:00:33	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE	64.0000	PV ALARM	HIGH	22.0000		
10/04/05 14:59:38	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	22.0000		
10/04/05 14:59:01	Alarm01	ALARM	CONTROL	TRN	CONTROL	SANDBATH 2 HD SP	480.2718	PV ALARM	HIGH	100.0000		
10/04/05 14:58:49	Alarm01	ALARM	CONTROL	TRN	CONTROL	SANDBATH 2 HD SP	50.2000	PV ALARM	HIGH	RETURN		
10/04/05 14:35:48	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		
10/04/05 14:35:34	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	CLD001	DIGALARM	STATE	RETURN		
10/04/05 14:34:24	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		
10/04/05 14:34:25	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	RETURN		
10/04/05 15:00:25	Stella	ALARM	CONTROL	SLPWSHT	ALARM01	SLOP TANK WEIGHT	5545.952	PV ALARM	HIGH	6000.000		
10/04/05 15:00:23	Stella	ALARM	CONTROL	SLPWSHT	ALARM01	SLOP TANK WEIGHT	4630.028	PV ALARM	HIGH	RETURN		
10/04/05 15:36:18	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	RETURN		
10/04/05 15:35:48	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	LOW	RETURN		
10/04/05 15:35:28	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	98.0000		
10/04/05 15:34:44	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	15.0000		
10/04/05 15:31:23	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	34.0000	PV ALARM	HIGH	RETURN		
10/04/05 15:20:58	Alarm01	ALARM	CONTROL	TRN	ALARM01	MAX TEMP	32.0000	PV ALARM	HIGH	25.0000		
10/04/05 14:30:57	Stella	ALARM	CONTROL	R2TEMP.HD	ALARM01	R 2 TEMP HEAT REQ.	141.1301	PV ALARM	HIGH	125.0000		
10/04/05 14:25:18	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE 107 T994	RET.	PV ALARM	HIGH			
10/04/05 14:22:07	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE	200.7578	PV ALARM	HIGH	200.0000		
10/04/05 14:17:17	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE 8400038	RET	PV ALARM	HIGH			
10/04/05 14:16:18	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE CLOSED		DIGALARM	STATE			
10/04/05 14:09:27	Stella	ALARM	CONTROL	RITOTOP	ALARM01	TOP TEMPERATURE	94.0000	PV ALARM	HIGH	31.0000		
10/04/05 14:07:48	Stella	ALARM	CONTROL	RHCOOL.BV	ALARM01	R1 COOLANT BUX VALVE	OPEN	DIGALARM	STATE	OPEN		

Alarm Priority = **Critical**

Description = Waldo is
on the loose




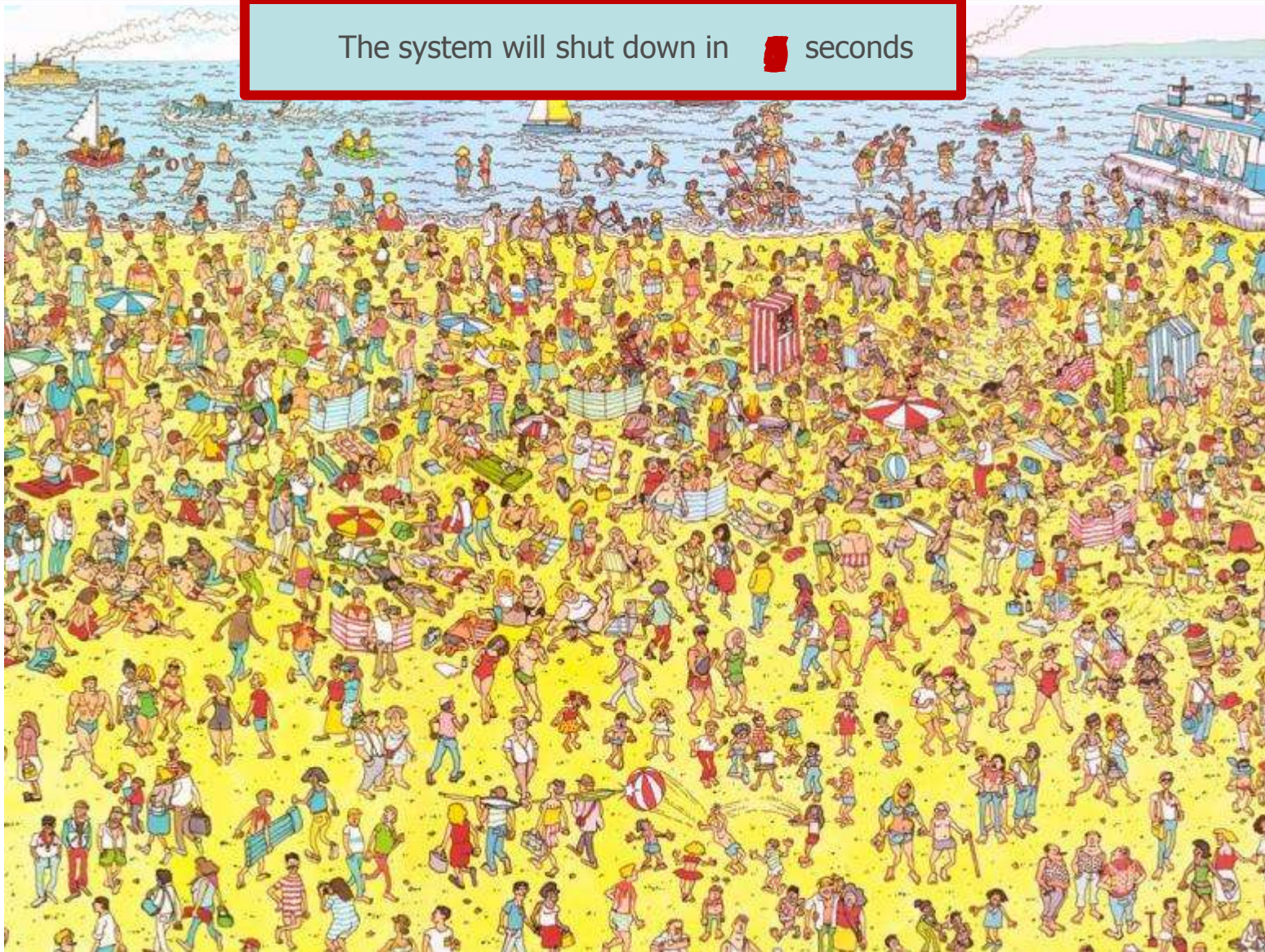
Alarm Management Best Practice:

Critical Alarm = an abnormal event with **SEVERE** consequences requiring **IMMEDIATE** action

Good luck!

Find Waldo...

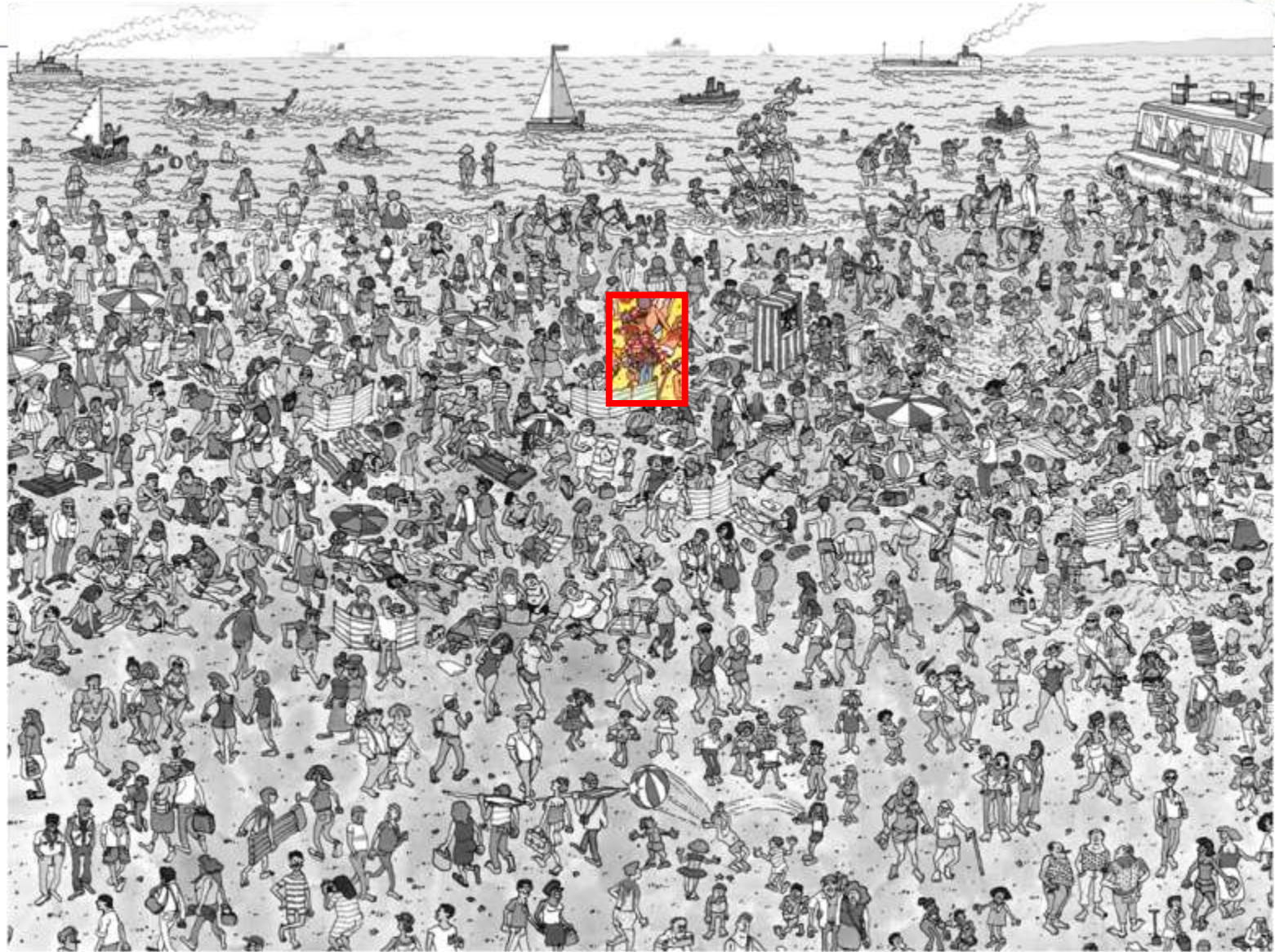
The system will shut down in  seconds



Lets Go to Grey Scale...



There he is...



Appropriate use of Color



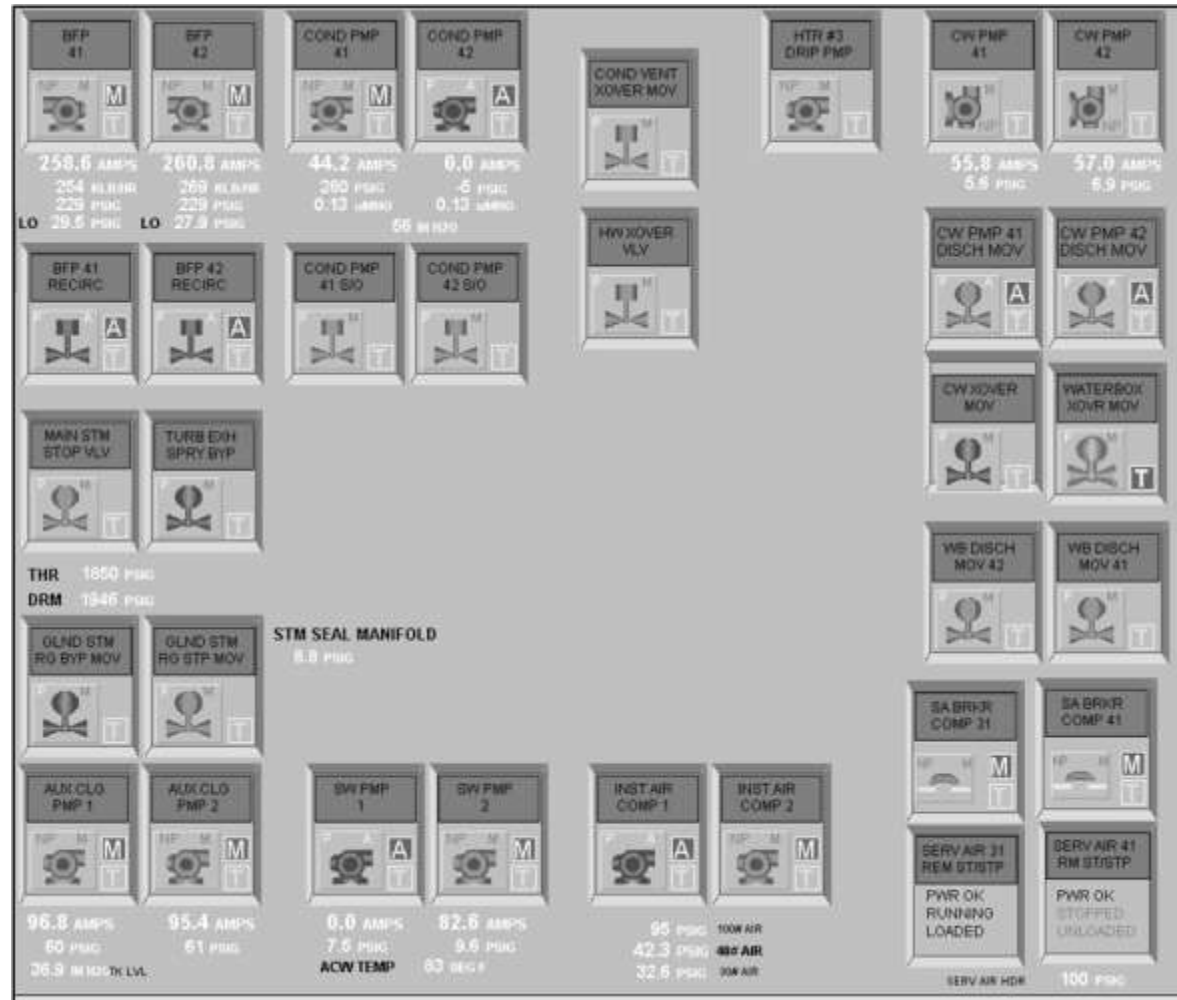
- Color is an attention getter.
- Use for the abnormal, not the normal.
- Screens should function even if the color is “turned down” – like an old television!



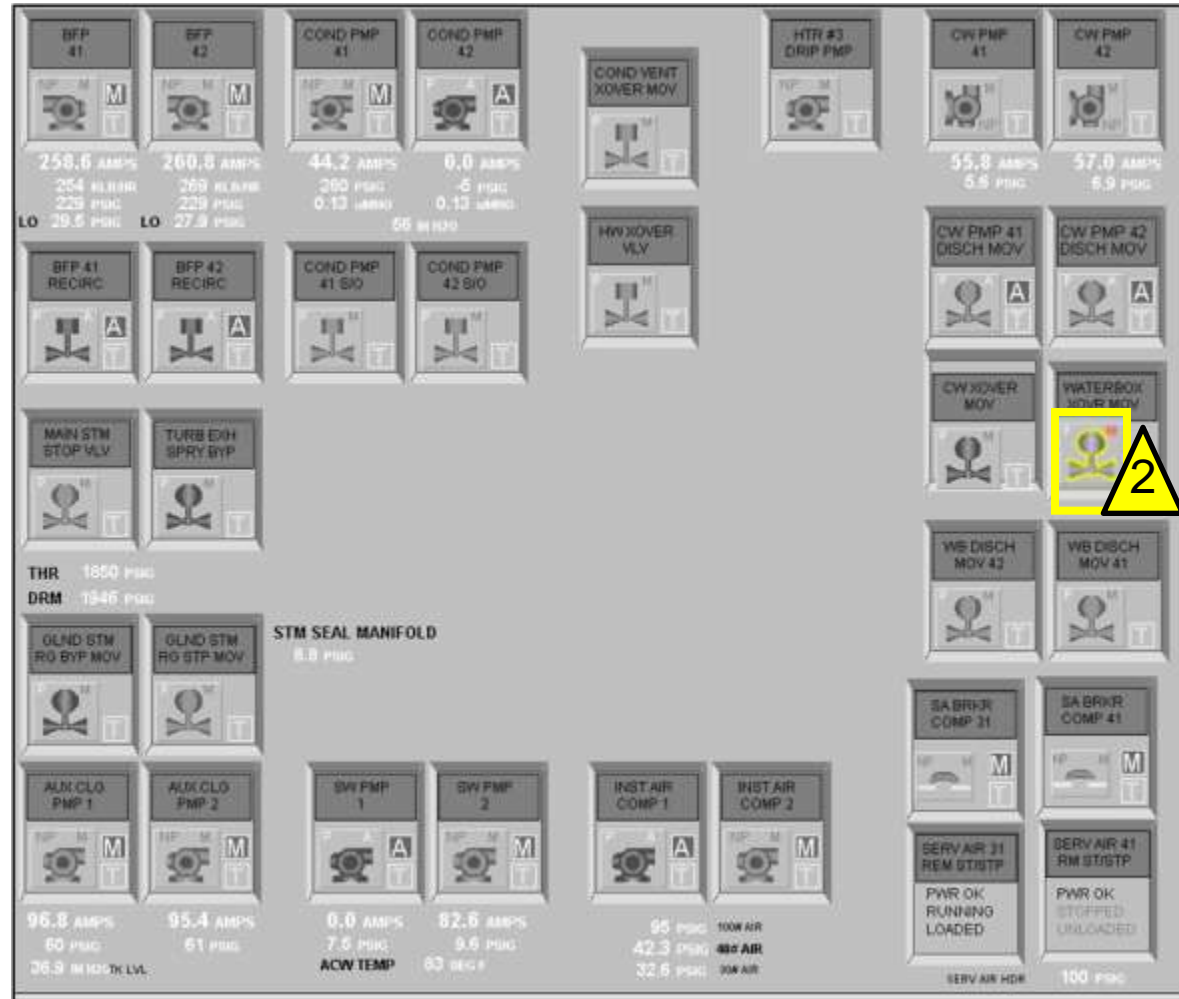
Lets Go to Grey Scale



- This is what the screen would look like for a color blind person
- About 6% of males in the US have certain amount of color blindness
- Can you tell which valves are open/closed in this display? Color blind people cannot tell the difference between red/green



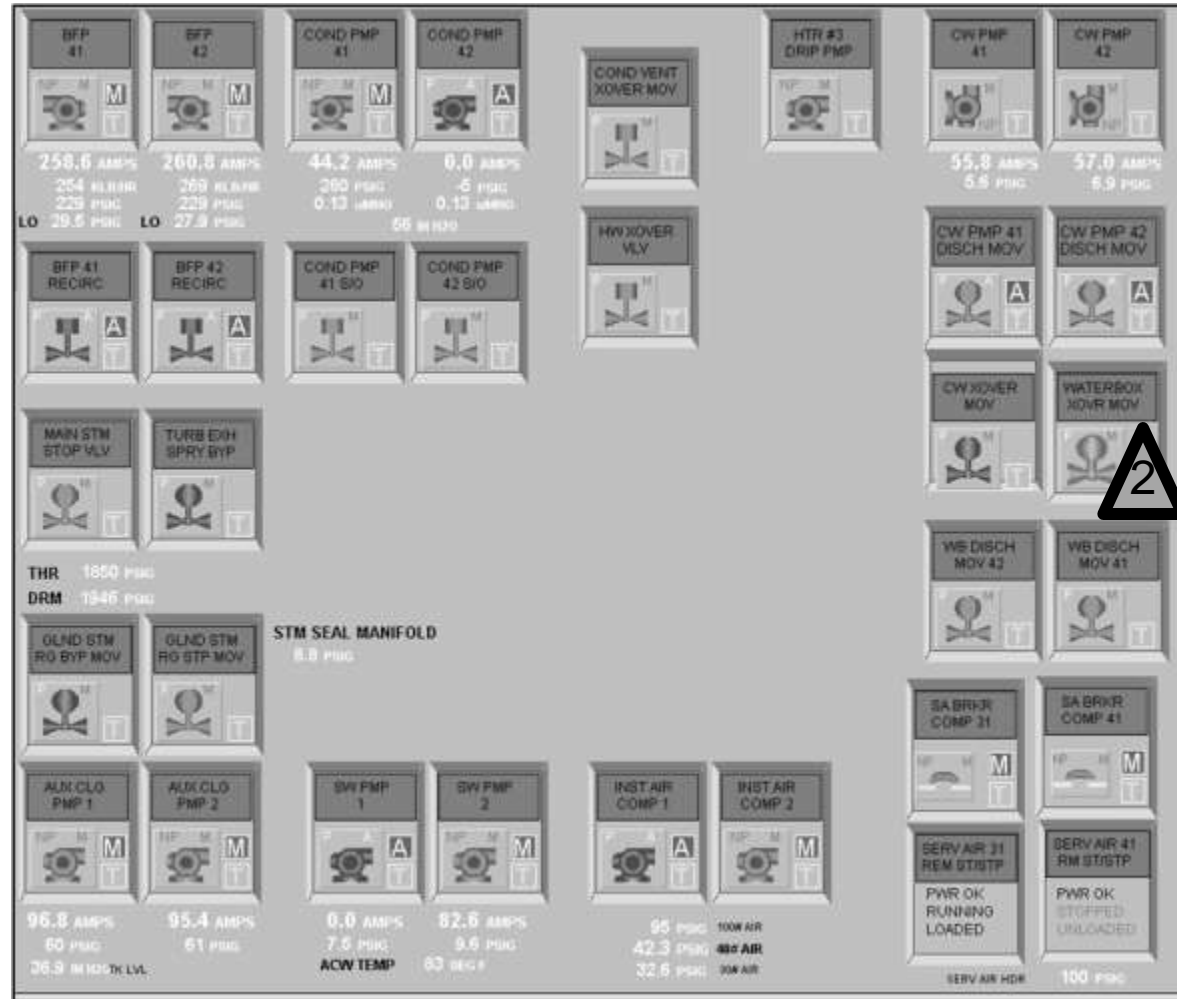
- Can you tell which valves are open/closed in this display? Color blind people cannot tell the difference between red/green
- Moral of the Story:
 - 1) Reserve bright colors for abnormal situations.
 - 2) Do NOT rely solely on color to depict important status indications– for alarms use Shape/Text and color (triple coding)



- Moral of the story:

- **SIMPLIFY**

- Appropriate use of color
- Animation for abnormal only

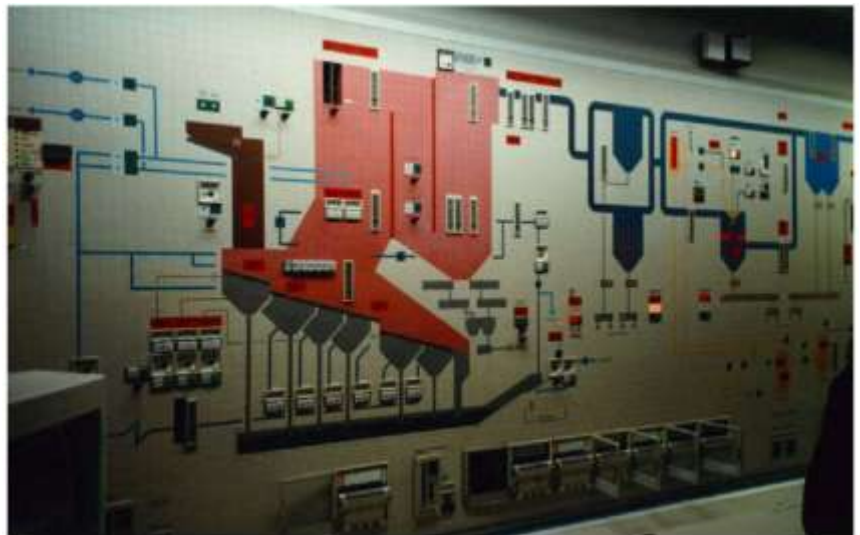


The High Performance HMI

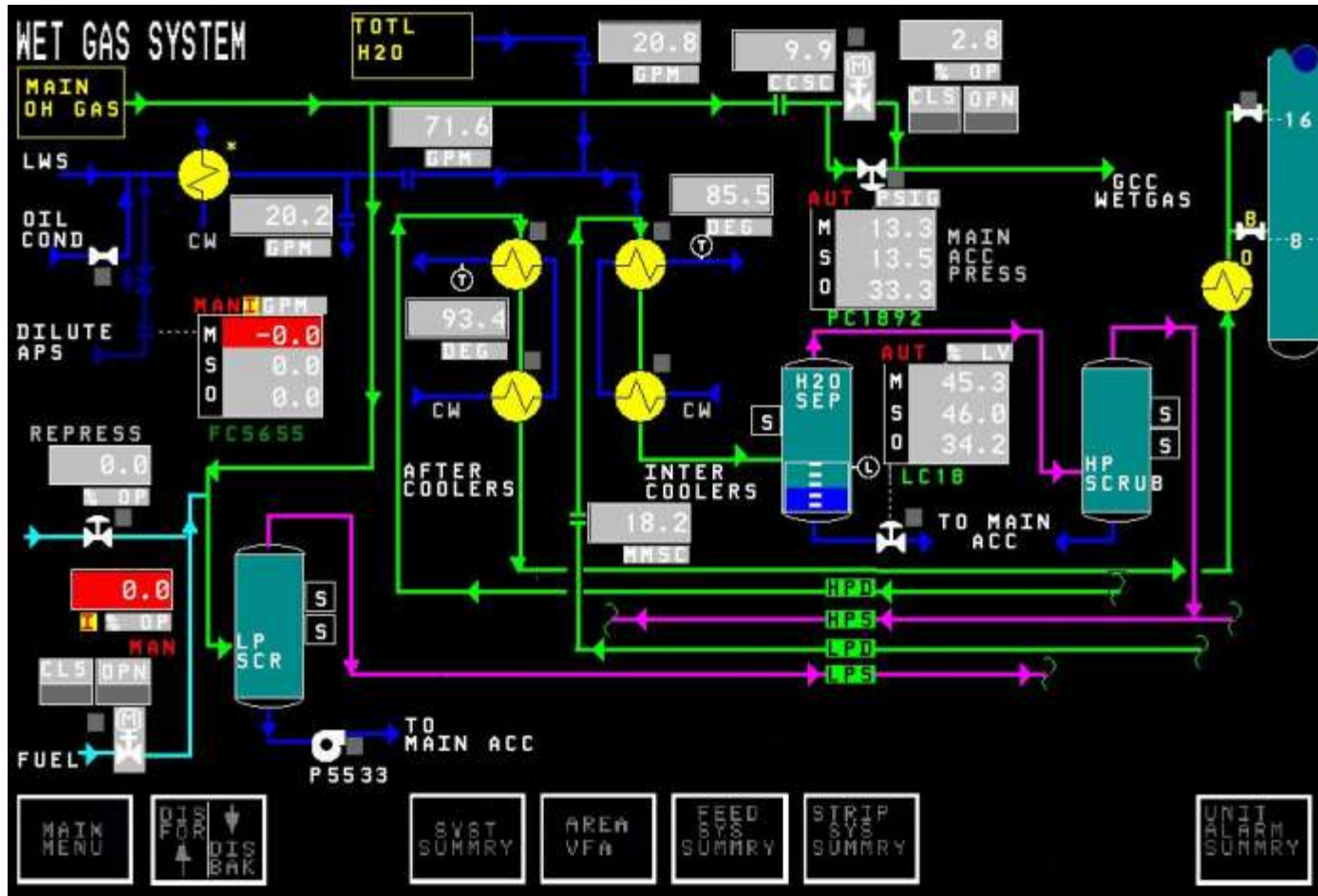
HMIs Past and Present



- Provided the “Big Picture”
- Limited Capability
- Many Process Trends
- Status “at-a-glance”



DCS Graphics Introduced – but no guidelines!



Traditional Graphics Encourage Poor Operating Practices

The High Performance HMI



- Time after time, poor HMIs are cited as contributing factors to major accidents
- \$800,000 per year savings anticipated on 1 ethylene plant
- Similar results for a PAS-EPRI study of a coal-fired power plant

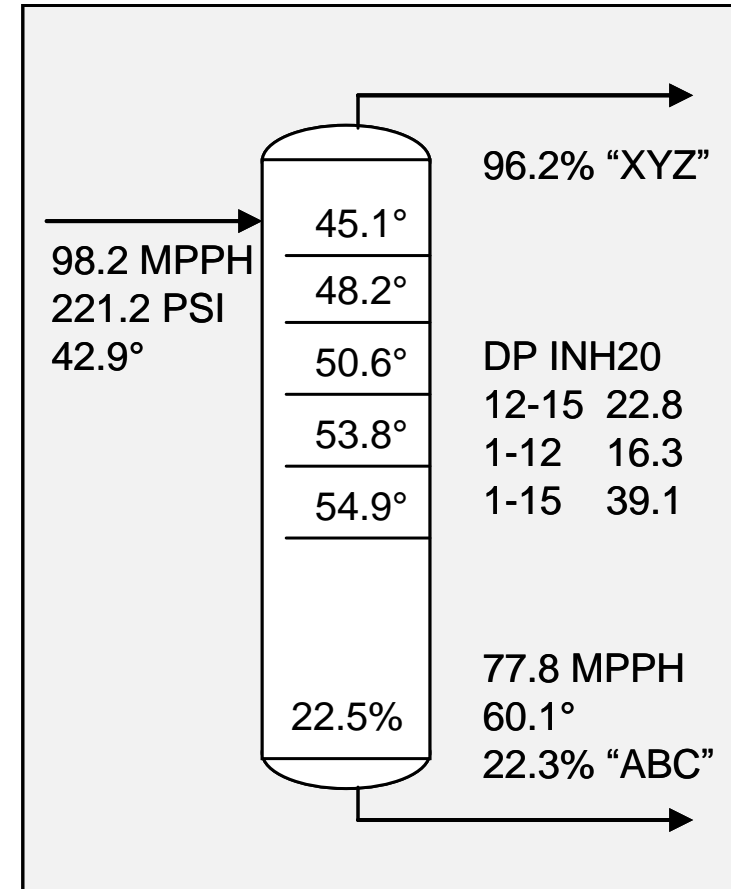
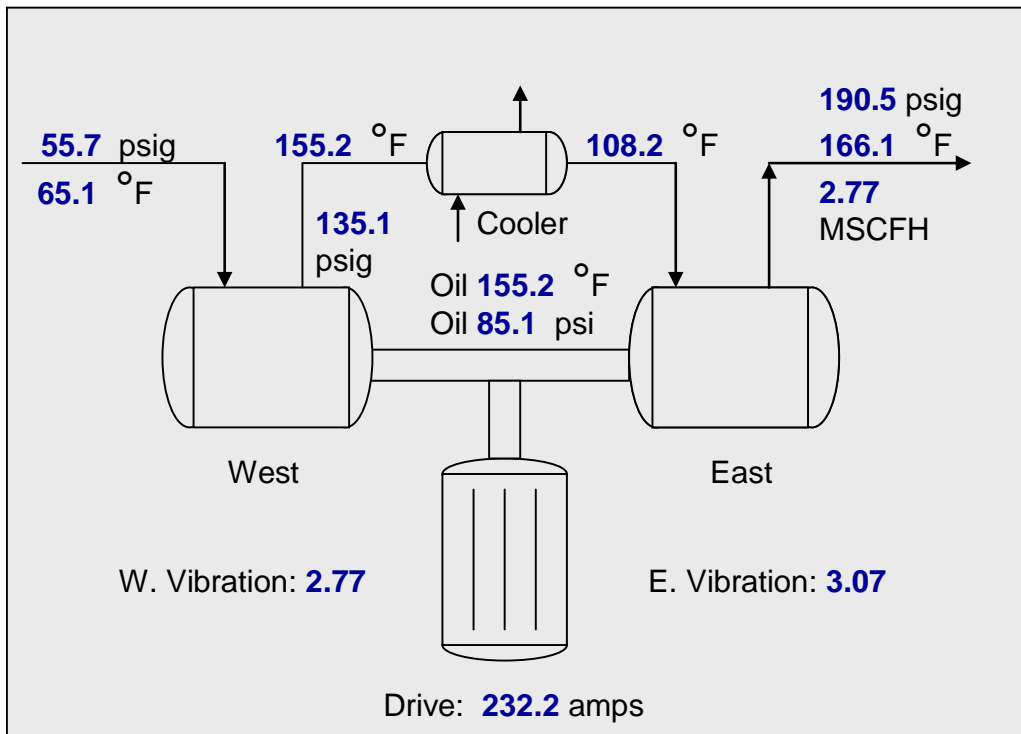
Task	Improvement
Detecting Abnormal Situations Before Alarms Occur	A 5X increase
Success Rate in Handling Abnormal Situation	37% over base case
Time to Complete Abnormal Situation Tasks	41% reduction

Study by Nova Chemicals and
ASM® Consortium

Data is Not Information



- Lots of Data but Not Much Information!
- Poor Presentation
- High Mental Workload to Decipher



P&IDs are NOT HMIs

Data is Not Information: Is Fluffy Sick?

Blood Tests for Fluffy -1	
Test	Results
HCT	31.7%
HGB	10.2 g/dl
MCHC	32.2 g/dl
WBC	$9.2 \times 10^9 /L$
GRANS	$6.5 \times 10^9 /L$
L/M	$2.7 \times 10^9 /L$
PLT	$310 \times 10^9 /L$



**Answer: Unless you
are a veterinarian,
how can you know?**

How About Now?



Blood Tests for Fluffy -3			
Test	Results	Range	Indicator Low – Normal - High
HCT	31.7%	24.0 – 45.0	
HGB	10.2 g/dl	8.0 – 15.0	
MCHC	32.2 g/dl	30.0 - 36.9	
WBC	9.2 x10 ⁹ /L	5.0 – 18.9	
GRANS	6.5 x10 ⁹ /L	2.5 – 12.5	
L/M	2.7 x10 ⁹ /L	1.5 – 7.8	
PLT	310 x10 ⁹ /L	175 - 500	

Contextualize information

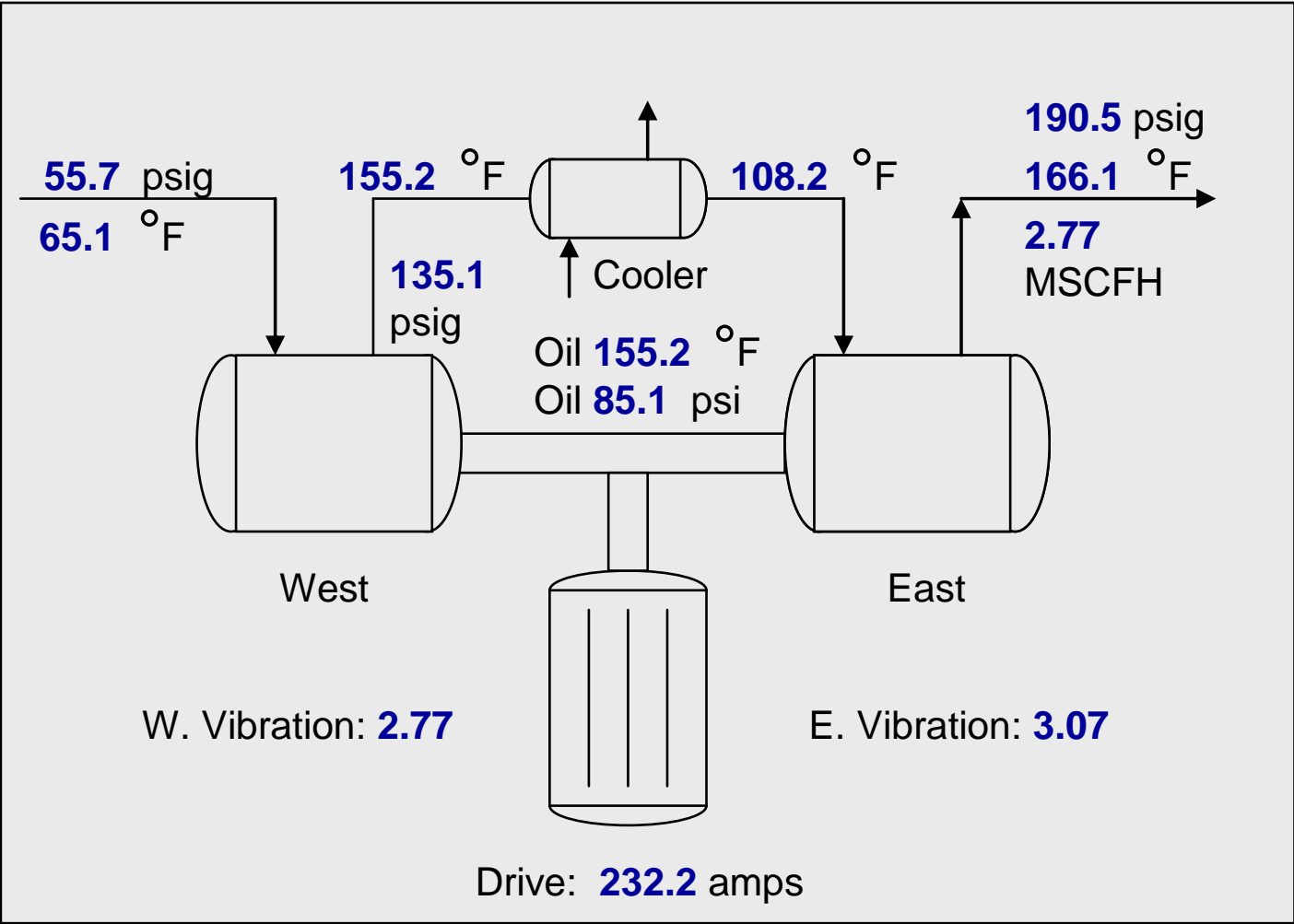
How About Now?



Blood Tests for Fluffy -3											
Test	Results	Range	Indicator Low – Normal - High								
HCT	31.7%	24.0 – 45.0									
<div style="border: 1px solid black; border-radius: 15px; padding: 10px; background-color: #e0f2f1;"> <p>Tag = HCT Alarm = PVHI The hematocrit (HCT) is the proportion, by volume, of the blood that consists of red blood cells</p> <table border="0"> <tr> <td>Causes</td> <td>Corrective Actions</td> </tr> <tr> <td>Temporary dehydration</td> <td>Drink water</td> </tr> <tr> <td>Lung Disease</td> <td>Lung exam</td> </tr> <tr> <td>Bone marrow disorder</td> <td>Bone marrow exam</td> </tr> </table> </div>				Causes	Corrective Actions	Temporary dehydration	Drink water	Lung Disease	Lung exam	Bone marrow disorder	Bone marrow exam
				Causes	Corrective Actions						
				Temporary dehydration	Drink water						
				Lung Disease	Lung exam						
				Bone marrow disorder	Bone marrow exam						
PLT	310 x10 ⁹ /L	175 - 500									

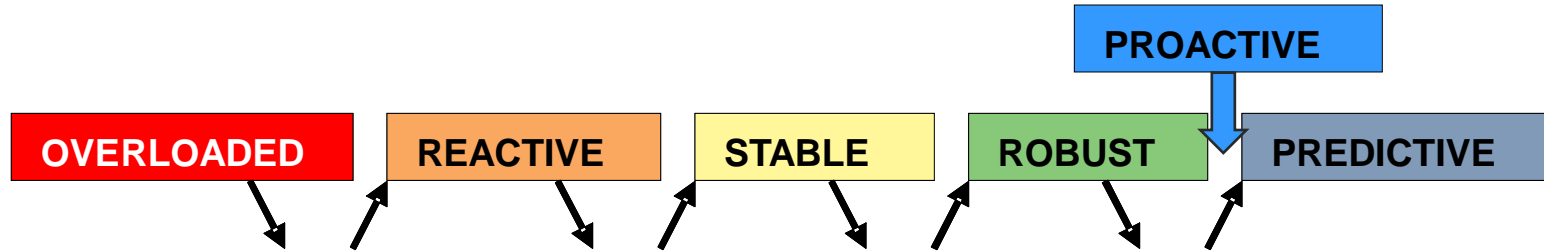
Aggregate information into the HMI

Analog in Industrial Examples



Is this compressor running OK?

From Robust to Proactive



Improvement Plans : Specific Steps to move from each classification to the next.

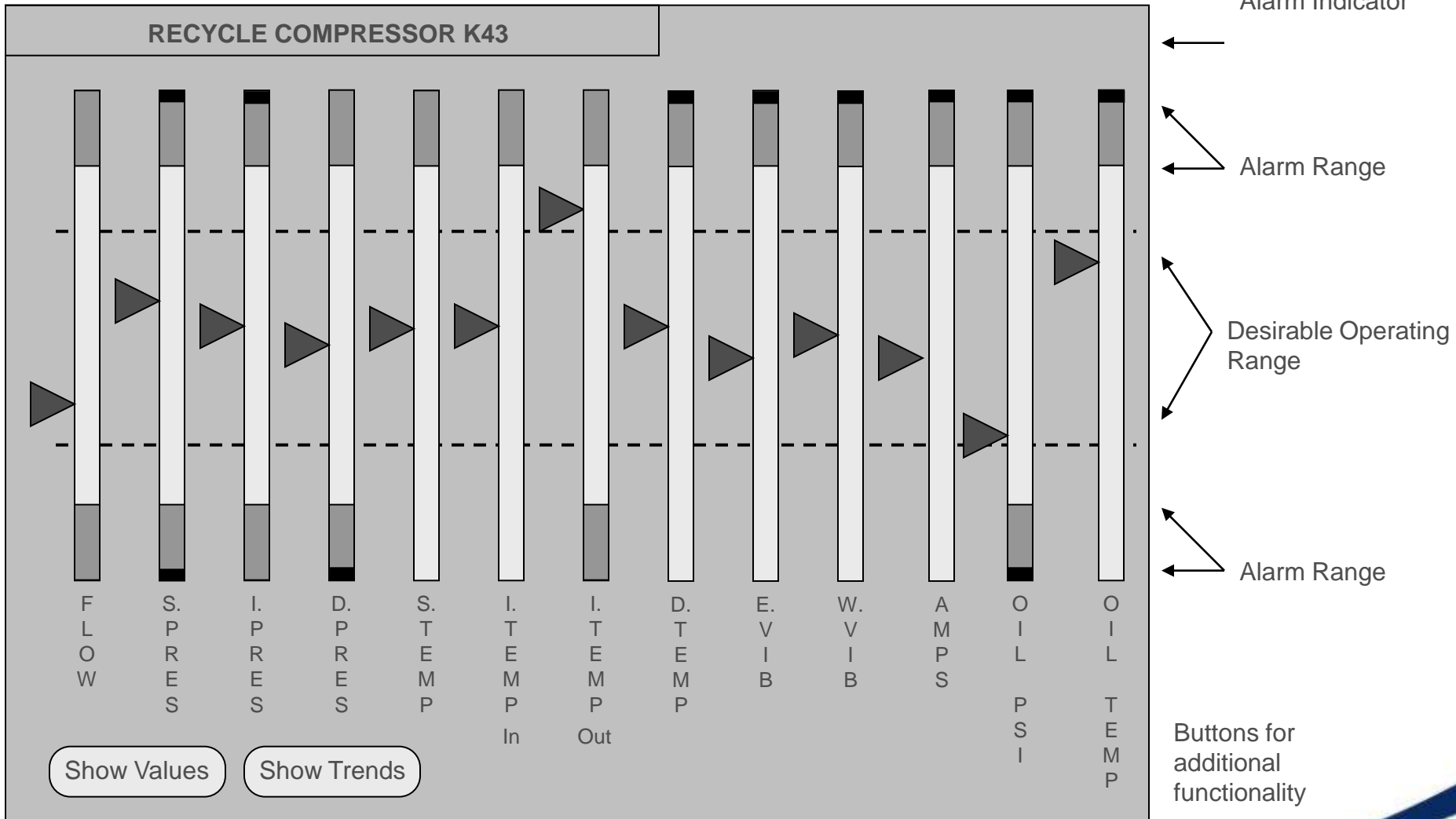
- **ROBUST**: Average and the peak alarm rates are under control for foreseeable plant operating scenarios
 - Dynamic and state-based techniques used to improve the real time performance
 - Alarm system is reliable during all plant modes, including normal operation and plant upsets
 - Operators have a high degree of confidence in the alarm system, and have time to detect and understand all alarms
 - Alarm system configuration is not subject to inadvertent change

Next Step: Enabling Operators to be Proactive

Analog in Industrial Examples



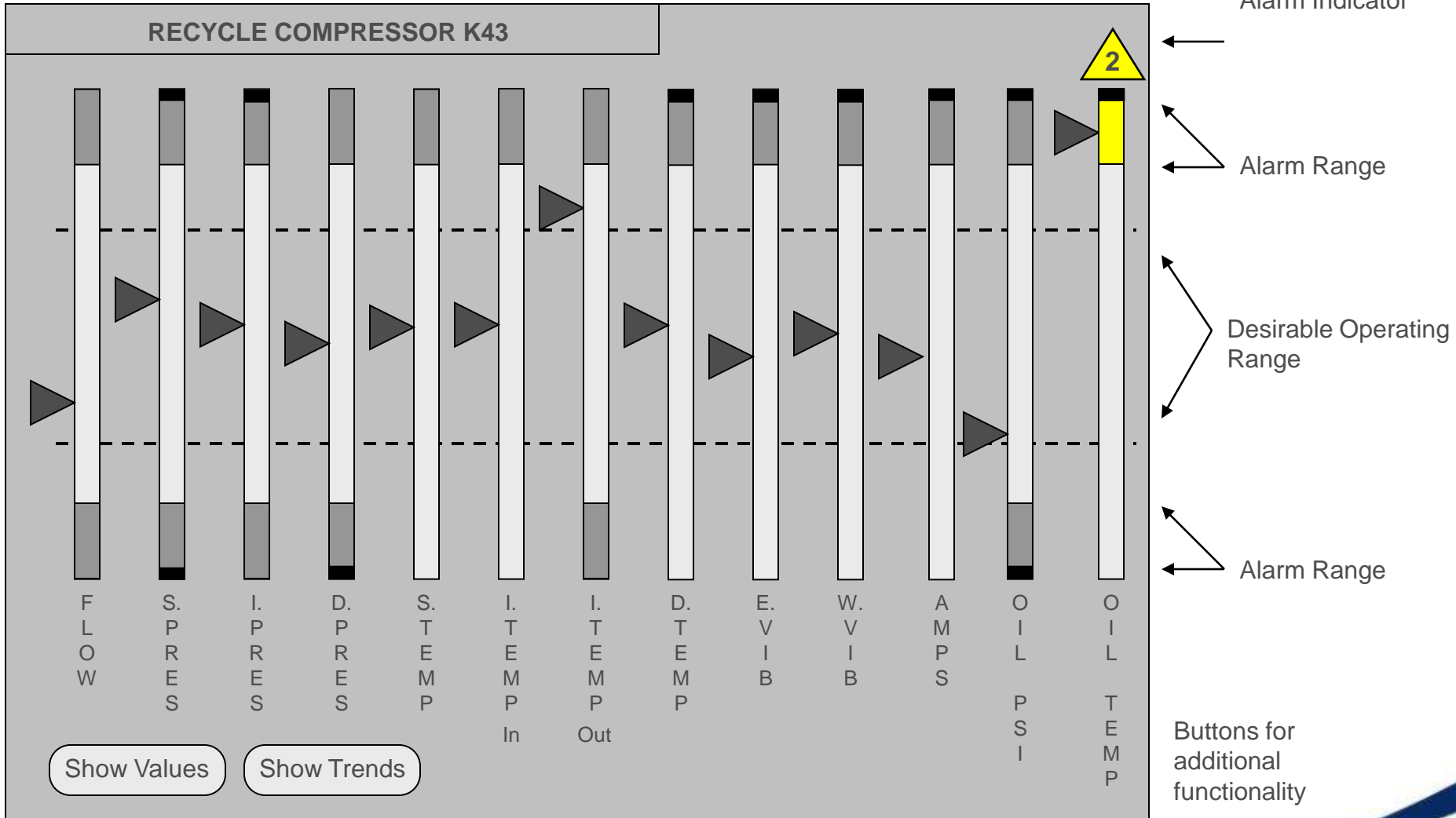
Compressor Status Showing Alarm/Shutdown Limits



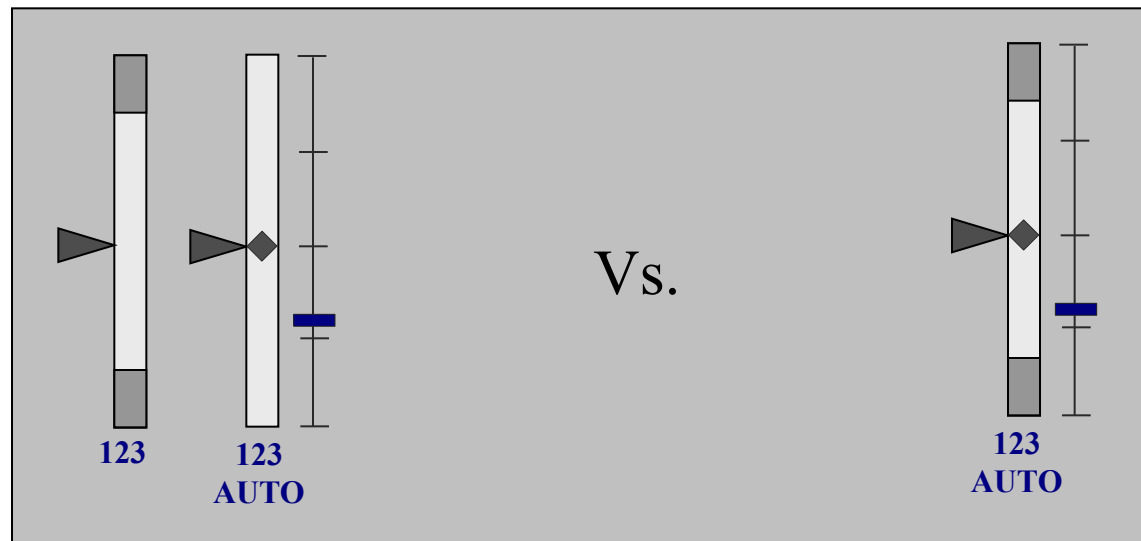
Analog in Industrial Examples



Compressor Status Showing Alarm/Shutdown Limits

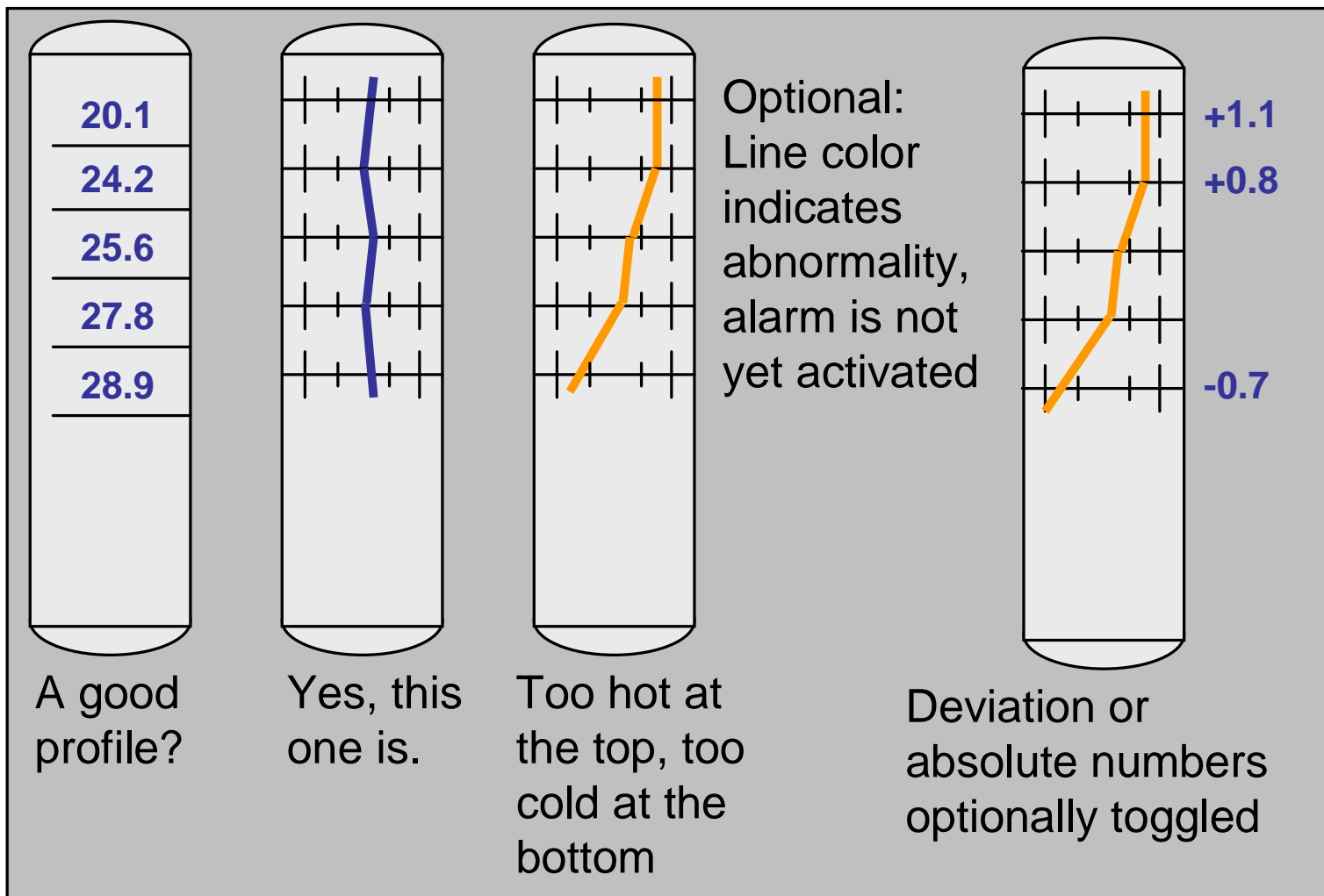


- Alarm management Best practice:
 - When indicators and controllers are available for one measurement, place alarms on controllers
- Effect on HMI:
 - Real Estate



**Proper Alarm Management Simplifies
Graphics Design**

Analog in Industrial Examples

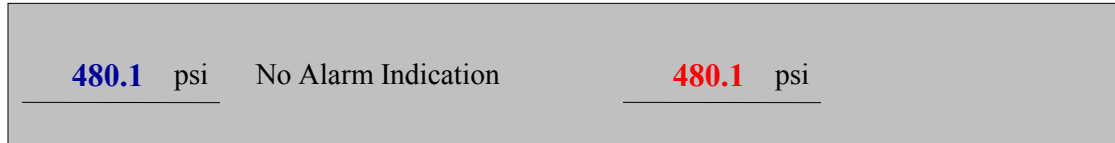


A Column Temperature Profile

Alarm Indications on Graphics

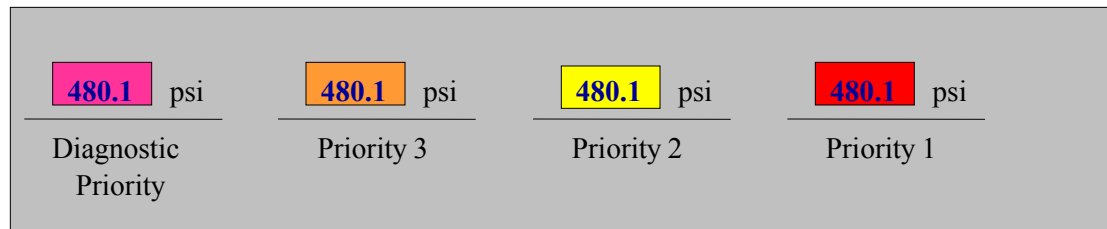


Worst

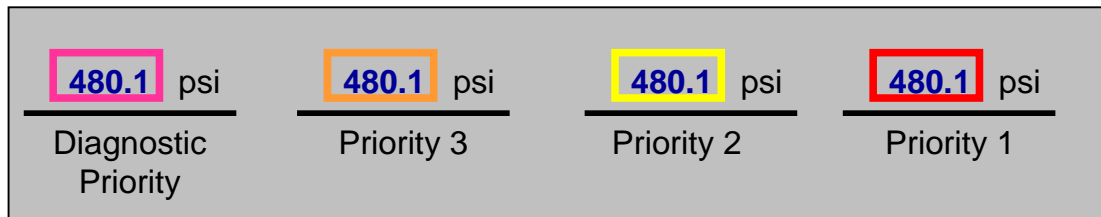


Only a Color Change!

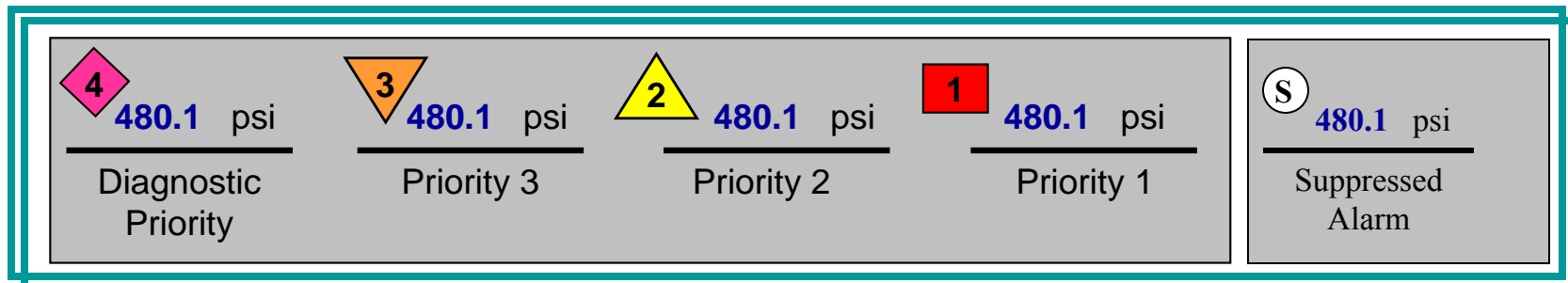
Poor



Poor

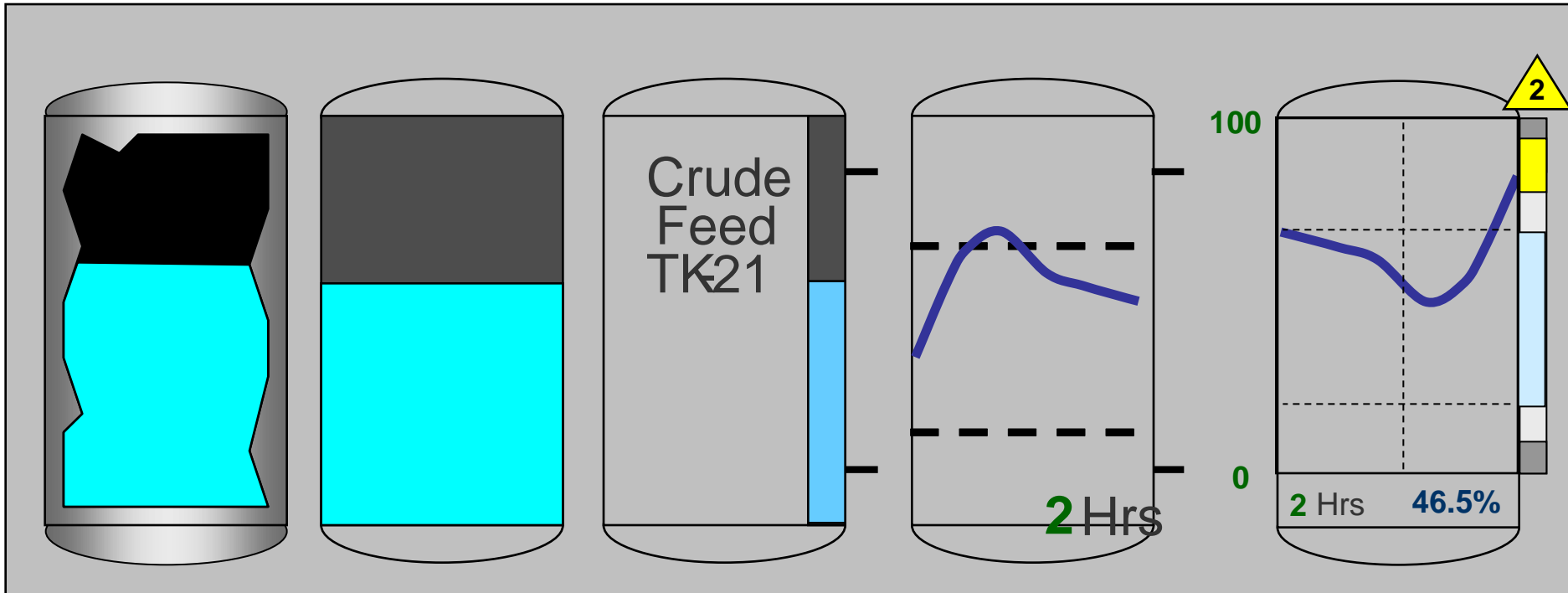


Best!



Multiple Coding: Color, Shape, Text

Level Depiction



Very Poor
Vessel
Level
Indication

Poor
Vessel
Level
Indication

Better
Vessel
Level
Indication

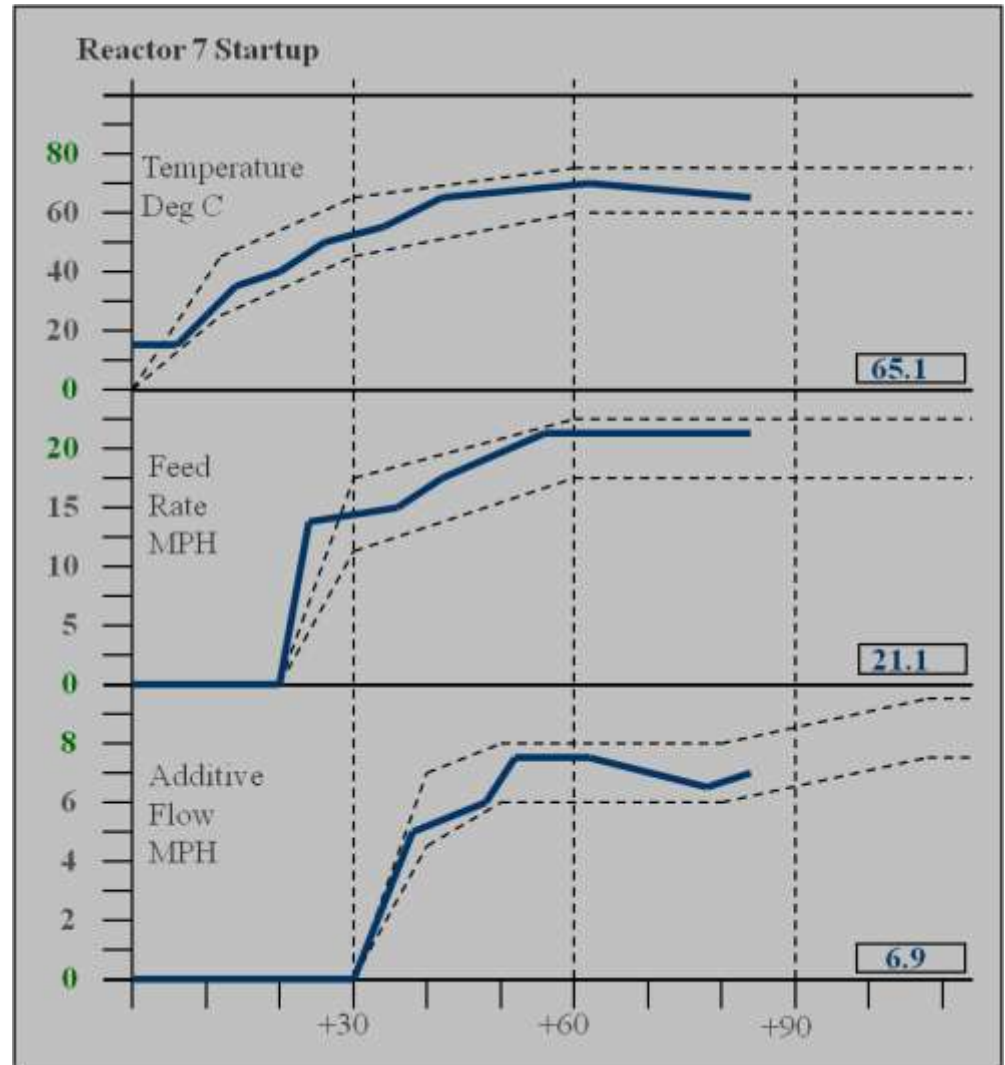
Trend
Vessel
Level
Indication

Combination
Vessel
Level
Indication

Custom Elements for Startups

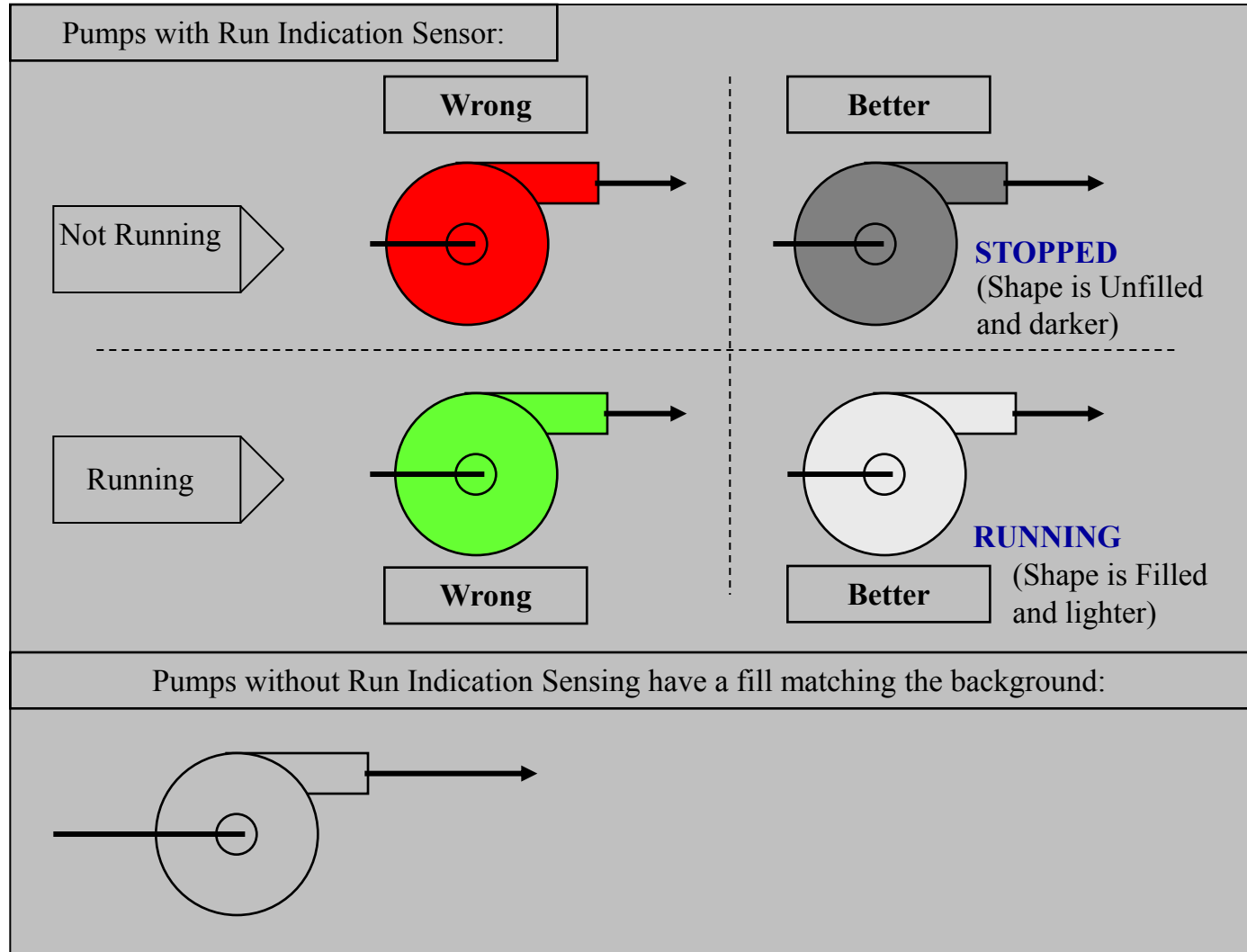


- Always try to clearly depict:
 - “Where am I?”
 - “How am I doing vs. what is “good?””



Status Depiction

- Bright color is used to indicate abnormal situations only



- HIERARCHY for Displays:
- Level 1 – Process Area Overview
 - Entire Operator Span of Control. “Single-Glance”
- Level 2 – Process Unit Control
 - Sub-unit controlled by operator
- Level 3 – Process Unit Detail
 - Equipment or controller
- Level 4 – Process Unit Support and Diagnostic Displays
 - Interlocks, ESDs, diagnostic screens, etc.

Level 1 Overview



Reactor 1

Run Plan:
Actual:

Comp A

Comp B

Cool

CPC

CRM

LVL

Prod: **Thionite**
State: **Mid-Run**
Agit: **ON**
Locks: **CLEAR**

Balance

IN

OUT

Rate

2 HR

Hydrog A

Cycle Comp A

Bed A1

Bed A2

Suct

Dsch

VIB: **OK**
BRG: **OK**
OIL: **OK**
Locks: **CLEAR**

500

F

L

O

W

470

2 HR

Key Performance Indicators

Conversion Efficiency

12 HR

Emissions Limit Ratio

Reactor 2

Run Plan:
Actual:

Comp A

Comp B

Cool

CPC

CRM

Rate

2 HR

Hydrog B

FC0001: E1002 BOTTOMS FLOW

- Shelf Alarm
- Operator Alert
- Alarm Details
- Loop Sheets: ▶
- SOP's: ▶
- Picture of FV402
- Notes: ▶
- Search

PAS Chemical, Inc. SOP500-R3.2
Houston, TX Reactor 2 SOP
Updated 23-Apr-2010

Standard Operating Procedure

Reactor 2 SOP

Table of Contents

- 1.0 Purpose of this document 2
- 2.0 Safety and Precautions 3
- 3.0 Special Equipment (PPE) 4
- 4.0 Prerequisites 5
- 5.0 Procedures 6
- 5.1 Start Feed 7
- 5.2 Start Compressor A & B 8
- 5.3 Start Agitator 9
- Figure 1 - Agitator 9
- 5.4 Start CRM flow 10
- 5.5 Start Additive 1 and Additive 2 11
- 5.6 Start Additive 1 and Additive 2 13
- 6.0 Critical Parameters 13
- 7.0 References 14

Alarms:	P1	P2	P3	P4
ACK	0	1	2	4
UNACK	0	0	1	1

▲ 07160808:55:07 RX2LOW CRM-QUALITY EXC

Trend Control

Sys

Sys

L2

L3

L4

Level 2



Feed Components: A - B - C

Main Feed
 P 76.8 MPH
 S 76.0
 O 88.5 %
 AUTO

Additive 1
 P 11.9 MPH
 S 12.0
 O 22.3 %
 AUTO

Additive 2
 P 4.0 MPH
 S 4.0
 O 44.3 %
 AUTO

Agitator **ON**

Reactor M5

Analysis: Purity %

Analysis: Inhibitor Concentration %

M5 Pressure
 P 98.0 psig
 S 95.0
 O 44.3 %
 AUTO

M5 Level %
 P 71.0 %
 S 70.0
 O 54.3 %
 AUTO

5.0 %

M5 Temp
 P 45.0 °C
 S 45.0
 O 54.3 %
 AUTO

Material Balance

IN OUT

19707 19301
 Calc Diff: 2.1 %
 Hours: 238.1
 Since: 06/02/07 14:00:00

Run Plan:

Actual:

Product: Thionite State: **Mid-Run**

SHUT DOWN M5

FREEZE M5

ISOLATE M5

Pumps Needed 1 Pump 1 **RUNNING** Diagnostics **1-OK 2-BAD** Pump 2 **STOPPED**

52.3 %

92.0 MPH PRODUCT

COOLING SYS

Temperature °C

COOLANT

Coolant Flow

Purge Rate

Cat. Activity

Coolant Temp

Conversion Efficiency

Reserve Capacity

Main Menu | Level 1 Reaction Overview | M4 | M6 | Trend Control | Feed System | Product Recovery | M5 Startup Overlay | M5 Sequence Overlay | - Level 3 - M5 Interlocks | - Level 3 - M5 Cooling System

OH → 20.1 psi → EAST COMP

WEST COMP RUNNING

WC Speed
P 90.8 %
S 90.0
O 90.0 %
CAS

Speed: 90.8

1 Stg psi: 48.0

2 Stg psi: 90.0

CLR In: 65.0

CLR Out: 32.0

Winding Temp: 111.0

SHOW / HIDE VALUES

NORMALIZE SCALE

Flow Demand
P 76.8 MSCFH
S 76.0
O 88.5 %
AUTO

SPEED CASCADE IN EFFECT

48.0 psi 65.0 °C → 1st Stage → 2nd Stage → 44.0 °C → 90.0 psi 48.4 MSCFH → EAST COMP → RECOVERY

West Compressor

IDLE WEST COMP

PURGE WEST COMP

SHUT DOWN WEST COMP

Initiator	Value	Action	Status
Overspeed	OK	Shut Down West Comp AND	
Or Winding Temp High	OK		
Or Vibration High	OK	Close Inlet & Outlet Block Valves AND	
Or 1 Stg High Pres	OK		
Or 2 Stg High Press	OK		
Or Suction Pres Low	OK	Override East Comp Speed to 100%	
Or Oil Pres Low	OK		

Main Menu

Compression Level 2

East Comp

Trend Control

OH System

Product Recovery

West Startup Overlay

West Sequence Overlay

Comp Cooling System

- Level 4 - Procedures

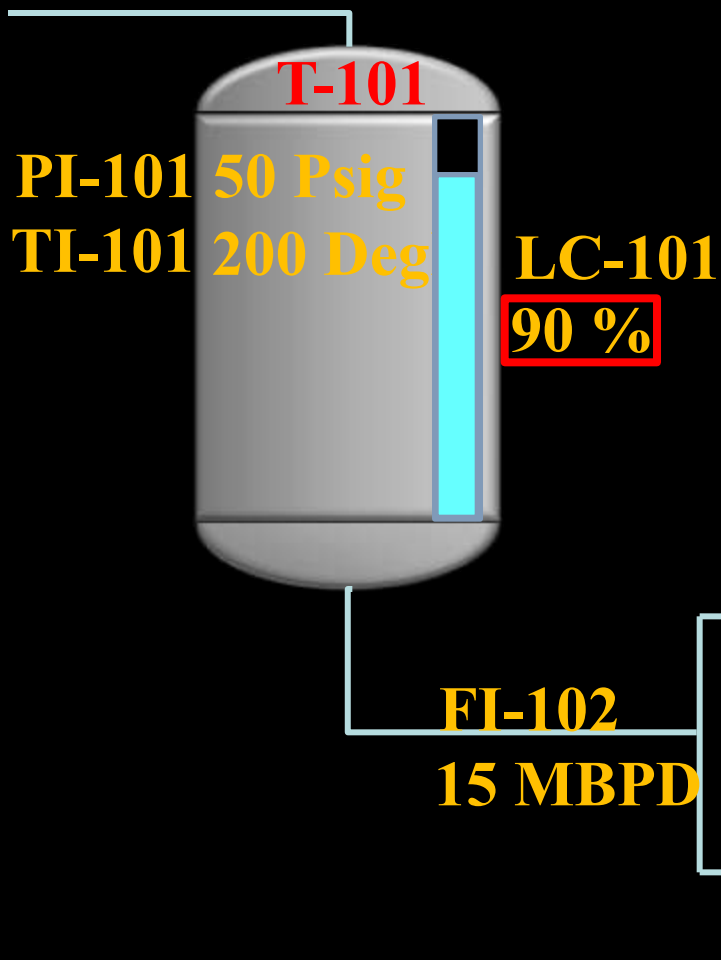
7 Steps for Creating High Performance Displays

1. Adopt a High Performance HMI Philosophy and Style Guide
2. Assess and benchmark existing graphics against the HMI Philosophy
3. Determine specific performance and goal objectives for the control of the process, for all modes of operation
4. Perform task analysis to determine the control manipulations needed to achieve the performance and goal objectives
5. Design and build high performance graphics, using the design principles in the HMI Philosophy and elements from the Style Guide, to address the identified tasks
6. Install, commission, and provide training on the new HMI
7. Control, maintain, and periodically reassess the HMI performance

Questions

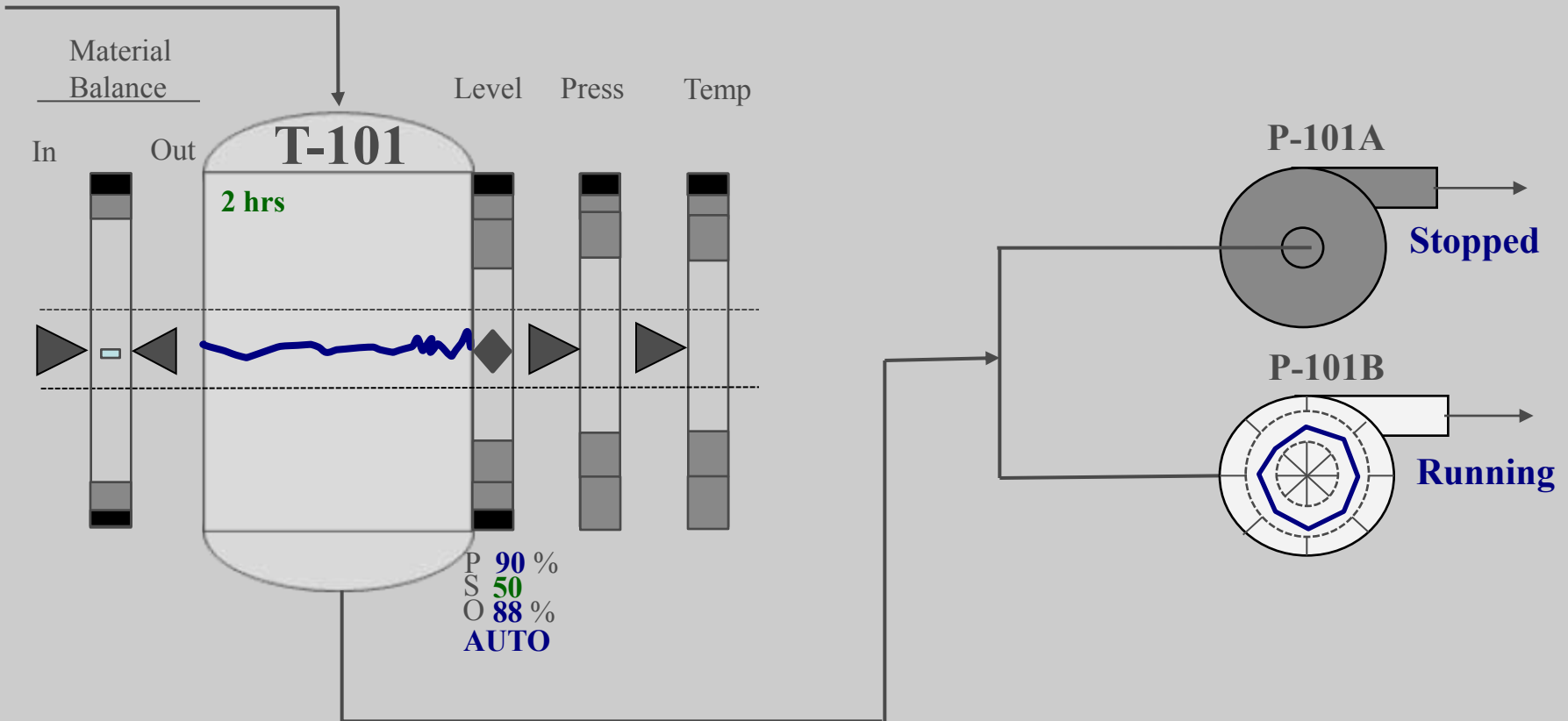


HP HMI 7 Steps Example



Pump Diagnostics	P-101 A	P-101B
Suction Pressure	60 PISG	40 PSIG
Disch. Pressure	1 PSIG	60 PSIG
Lube Oil Temp	120 DegF	120 DegF
Lube Oil Press.	20 PSIG	20 PSIG

HP HMI 7 Steps Example



HP HMI 7 Steps Example

